

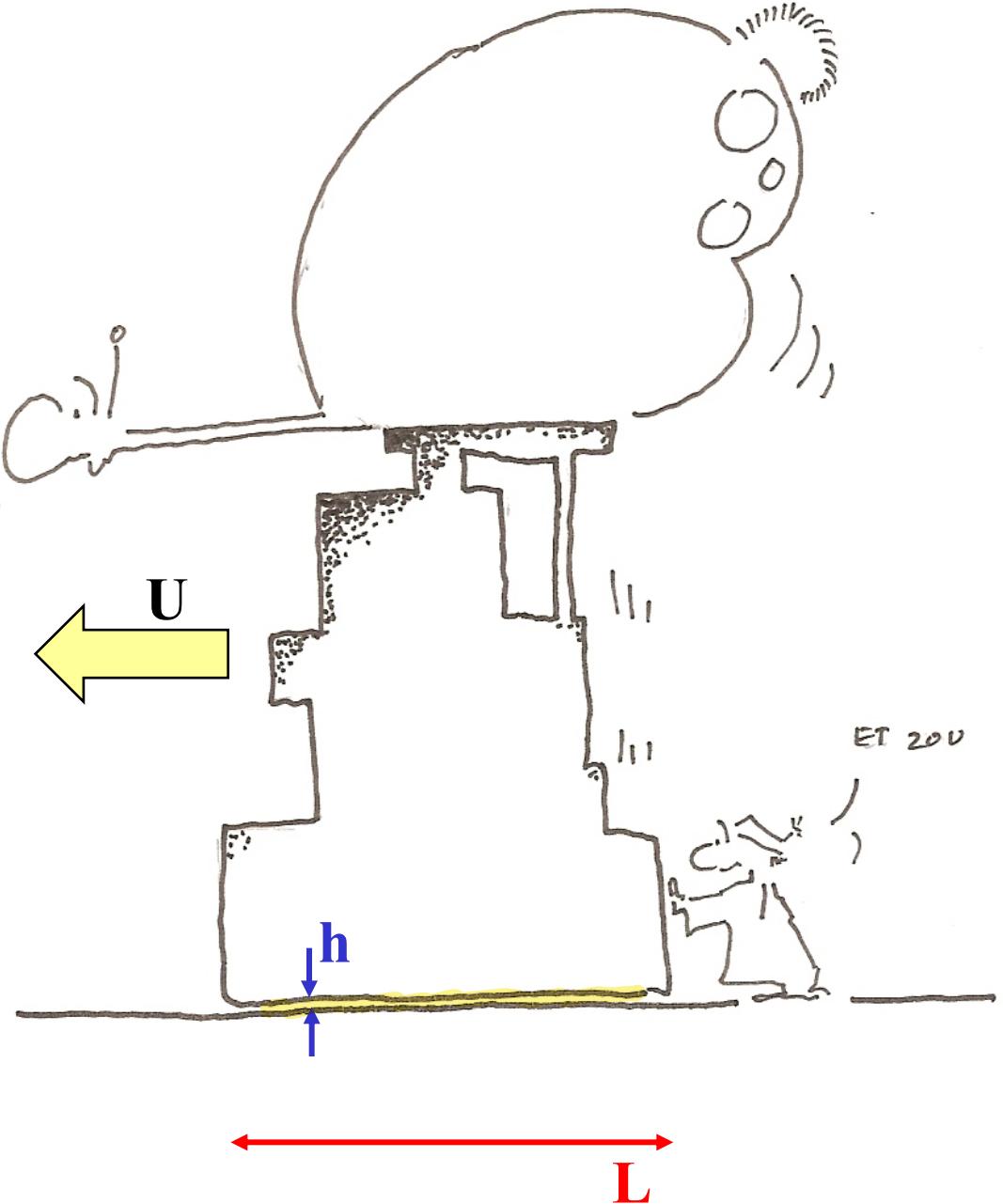
*Convection naturelle
le long d'une plaque
verticale : écoulement
laminaire permanent*

Mais que faire pour
des écoulements avec
deux échelles
spatiales ?



*Lubrification et convoyage
hydraulique : butée Michell*

Théorie de la lubrification

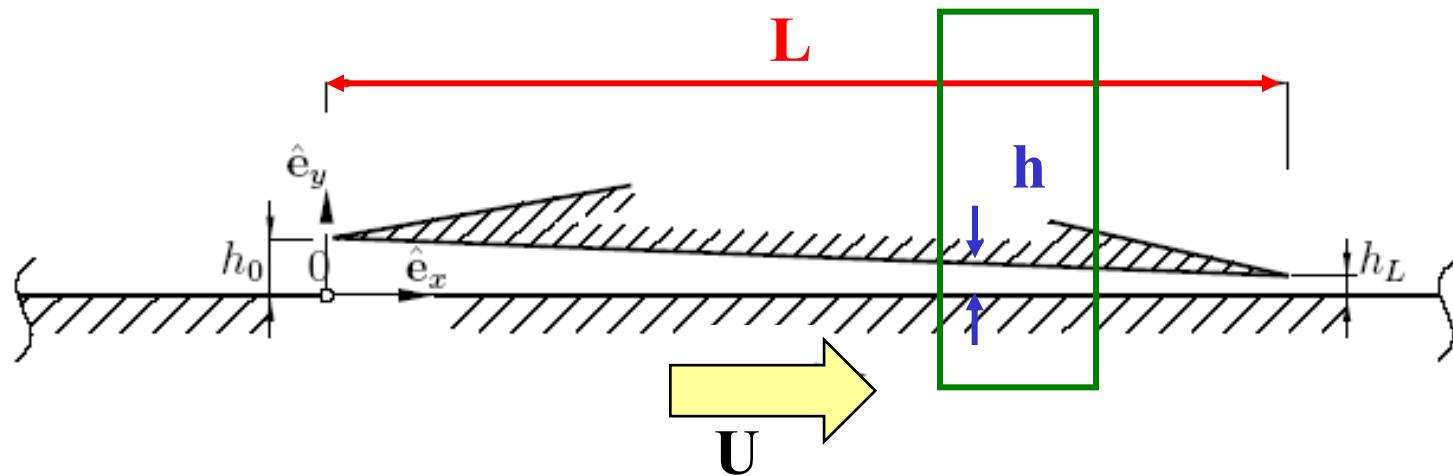
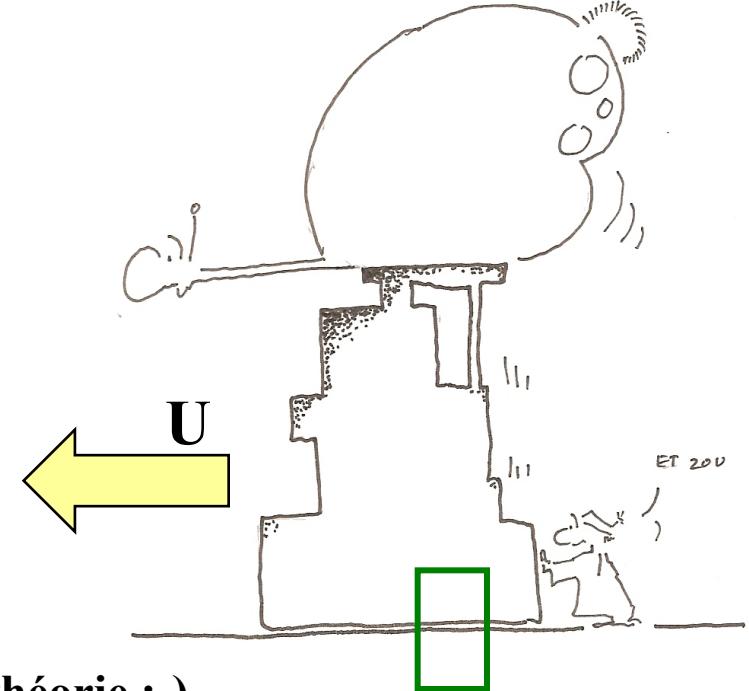


Convoyage hydraulique de charges très importantes :
- turbines hydroélectriques
- applications marines
- butées hydrauliques

Théorie de la lubrification

$$h \ll L$$

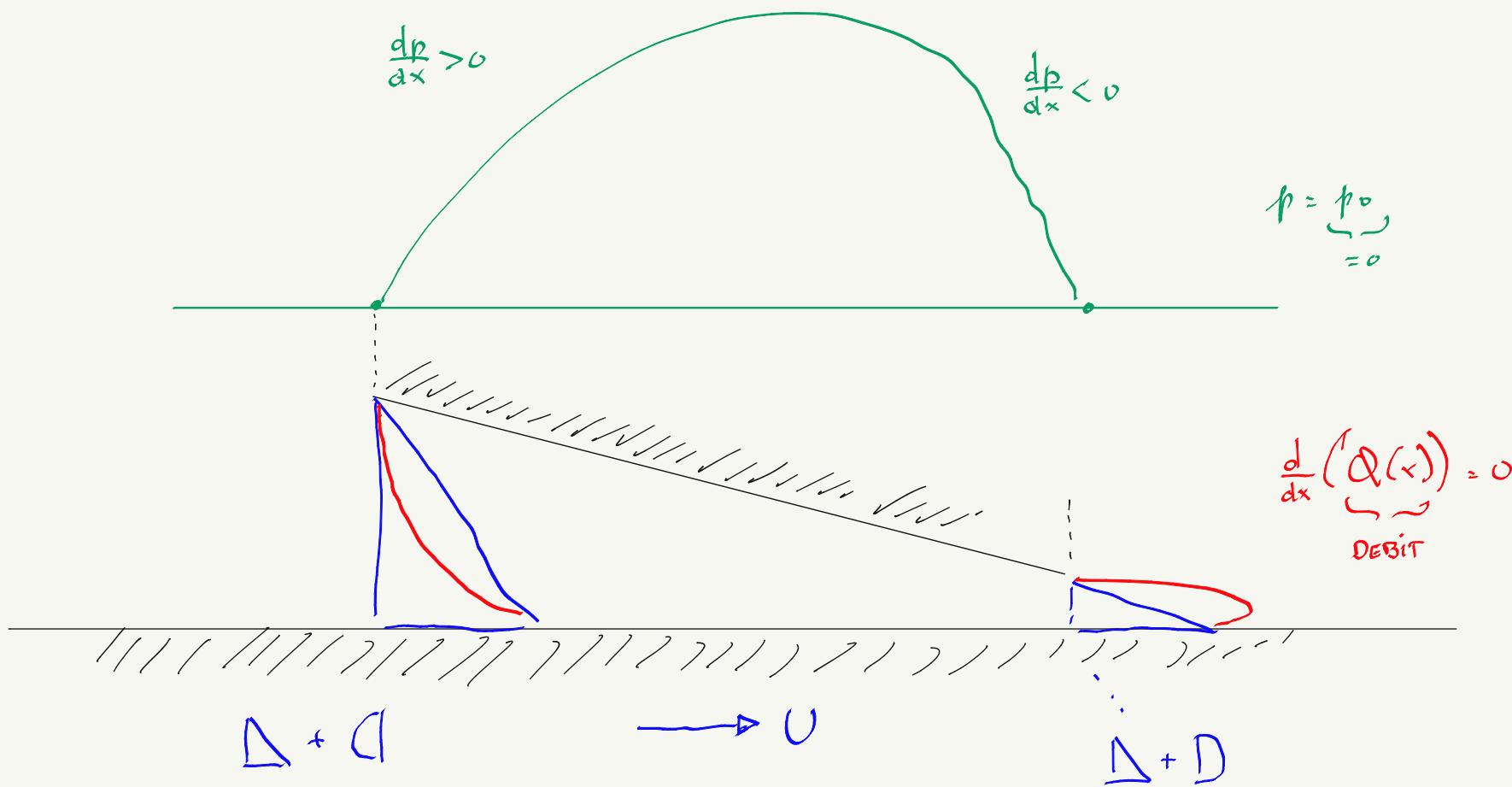
Hypothèse géométrique de base
Valable dans la zone centrale uniquement en théorie :-)



1

INTUITIVEMENT ?

ÉCOULEMENT INCOMPRESSIBLE
STATIONNAIRE



**Ecoulements
incompressibles
plans
stationnaires**

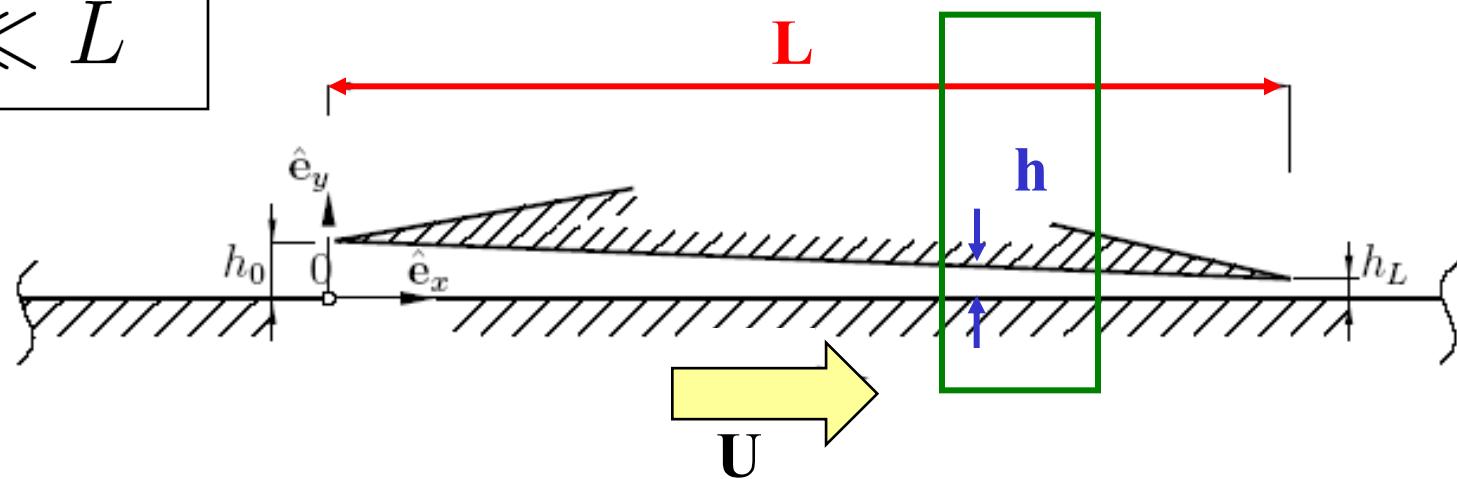
$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$\rho u \frac{\partial u}{\partial x} + \rho v \frac{\partial u}{\partial y} = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial x^2} + \mu \frac{\partial^2 u}{\partial y^2}$$

$$\rho u \frac{\partial v}{\partial x} + \rho v \frac{\partial v}{\partial y} = -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial x^2} + \mu \frac{\partial^2 v}{\partial y^2}$$

Que deviennent ces équations ?

$$h \ll L$$



$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$\rho u \frac{\partial u}{\partial x} + \rho v \frac{\partial u}{\partial y} = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial x^2} + \mu \frac{\partial^2 u}{\partial y^2}$$

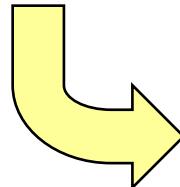
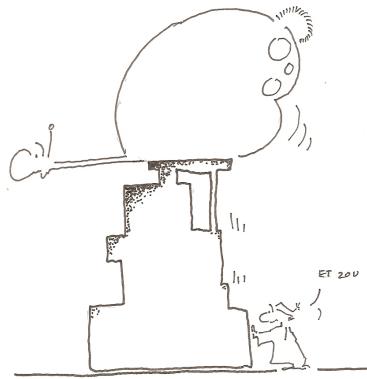
$$\rho u \frac{\partial v}{\partial x} + \rho v \frac{\partial v}{\partial y} = -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial x^2} + \mu \frac{\partial^2 v}{\partial y^2}$$

$$h \ll L$$

Longueur horizontale caractéristique : L

Longueur verticale caractéristique : h

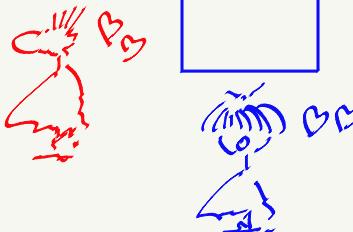
Vitesse horizontale caractéristique : U



Comment choisir une
vitesse verticale
caractéristique ?

2

DEFINIR
UNE VITESSE
VERTICALE
CARACTERISTIQUE :-)

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$


JE L'AI
DEDUIT
DE $h \ll L$

$$\frac{U}{L} = \frac{V}{h}$$

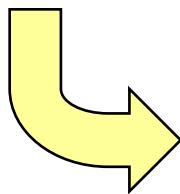

$$V = \frac{h}{L} U \ll U$$

$\ll 1$

$$\boxed{\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y}} = 0$$

$$\boxed{\mathcal{O}(U/L)} \quad \boxed{\mathcal{O}(V/h)}$$

Il ne faut pas définir de vitesse caractéristique verticale !



$$V = \frac{Uh}{L} \ll U$$

3

SIMPLIFICATIONS !

$$\cancel{\rho v \frac{\partial u}{\partial x}} + \cancel{\rho v \frac{\partial u}{\partial y}} = - \frac{\partial p}{\partial x} + \mu \cancel{\frac{\partial^2 u}{\partial x^2}} + \mu \frac{\partial^2 u}{\partial y^2}$$

$\cancel{\partial(\rho U^2/L)}$ $\cancel{\partial(\rho VU/h)}$

$$\cancel{\partial(\mu U/L^2)} \ll \cancel{\partial(\mu U/h^2)}$$

$$V = \frac{Uh}{L} \quad \left\{ \begin{array}{l} \\ \end{array} \right. \quad \cancel{\partial(\rho \frac{Uh}{L} \frac{U}{h})} = \cancel{\partial(\rho \frac{U^2}{L})}$$

$$\frac{\text{INERTIE}}{\text{VISCOSITE}} = \frac{\rho \frac{U^2}{L}}{\mu \frac{U}{h^2}} = \underbrace{\rho \frac{UL}{\mu}}_{\text{Re}} \underbrace{\frac{h^2}{L^2}}_{\text{Re}} \ll 1$$



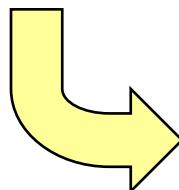
EN SUPPOSANT
QUE LE Re RESTE
ACCEPTABLE !

Quand peut-on négliger les termes d'inertie ?

$$\cancel{\mathcal{O}(\rho U^2/L)} \left(\rho u \frac{\partial u}{\partial x} + \rho v \frac{\partial u}{\partial y} \right) = - \frac{\partial p}{\partial x} + \mu \cancel{\frac{\partial^2 u}{\partial x^2}} + \mu \frac{\partial^2 u}{\partial y^2}$$

$\mathcal{O}(\rho VU/h) \quad \mathcal{O}(\mu U/L^2) \ll \mathcal{O}(\mu U/h^2)$

*Hypothèse de lubrification :
Écoulements rampants*



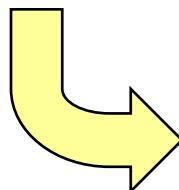
$$\frac{\text{Forces d'inertie}}{\text{Forces visqueuses}} = \frac{\rho U^2 / L}{\mu U / h^2} = \underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

Et l'autre équation ?

$$\cancel{\mathcal{O}(\rho U^2 h / L^2)} \left(\rho u \frac{\partial v}{\partial x} + \rho v \frac{\partial u}{\partial y} \right) = - \frac{\partial p}{\partial y} + \mu \cancel{\frac{\partial^2 v}{\partial x^2}} + \mu \frac{\partial^2 v}{\partial y^2}$$

$\mathcal{O}(\mu U h / L^3) \ll \mathcal{O}(\mu U / L h)$

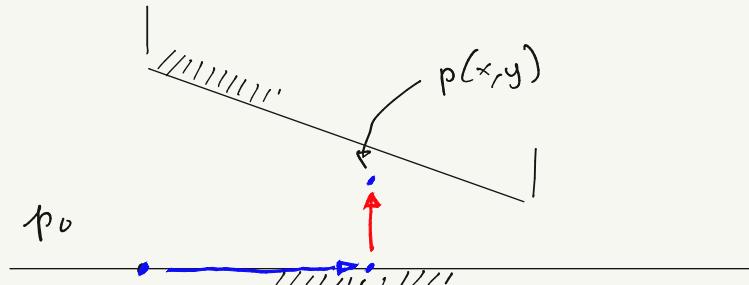
*On obtient la
même condition...*



$$\frac{\text{Forces d'inertie}}{\text{Forces visqueuses}} = \frac{\rho U^2 h / L^2}{\mu U / L h} = \underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

9

ET LA
PRESSION ?



$$p(x, y) - p_0 = \boxed{p(x, 0) - p_0} + \boxed{y \frac{\partial p}{\partial y} \Big|_{(x, 0)}} + y^2 \dots$$

\sim

c'est petit car $y^2 \ll y$

$$\partial(L) \quad \times \frac{\partial p}{\partial x} \quad \partial\left(\frac{\mu V}{h^2}\right) \quad \partial\left(\frac{\mu VL}{h^2}\right)$$

$$p(x, y) - p_0 = \boxed{p(x, 0) - p_0} + \boxed{y \frac{\partial p}{\partial y}(x, 0)} + y^2 \dots$$

c'est petit car $y^2 \ll y$

$\partial(h)$ $\partial(\frac{\mu V}{h^2})$

$\partial(L)$ $\times \frac{\partial p}{\partial x}$ $\partial(\frac{\mu V}{h^2})$ $\partial(\frac{\mu VL}{h^2})$

REYNOLDS

$$\frac{\partial v}{\partial x} + \frac{\partial r}{\partial y} = 0$$

$$\frac{dp}{dx} = \mu \frac{\partial^2 v}{\partial y^2}$$

THEORIE
DE LA
LUBRIFICATION

$$\frac{h^2}{L} \frac{\mu U}{L} \ll \frac{\mu UL}{h^2} \frac{h^2}{L}$$

$$\frac{h^2}{L^2} \sim \frac{\mu U}{L} \ll 1$$

$$\boxed{\cancel{\rho u \frac{\partial v}{\partial x}}} + \boxed{\cancel{\rho v \frac{\partial v}{\partial y}}} = -\frac{\partial p}{\partial y} + \boxed{\cancel{\mu \frac{\partial^2 v}{\partial x^2}}} + \boxed{\mu \frac{\partial^2 v}{\partial y^2}}$$

$\mathcal{O}(\mu U/Lh)$

Et la pression ?

$$p(x, y) - p_0 = \boxed{p(x, 0) - p_0} + \boxed{y \cancel{\frac{\partial p}{\partial y}}|_{y=0}}$$

$\mathcal{O}(\mu UL/h^2) \gg \mathcal{O}(\mu UL/L^2)$

↑

$$\boxed{\cancel{\rho u \frac{\partial u}{\partial x}}} + \boxed{\cancel{\rho v \frac{\partial u}{\partial y}}} = -\frac{\partial p}{\partial x} + \boxed{\cancel{\mu \frac{\partial^2 u}{\partial x^2}}} + \boxed{\mu \frac{\partial^2 u}{\partial y^2}}$$

$\mathcal{O}(\mu U/h^2)$

Equations de Reynolds (1889)

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

Théorie de la lubrification

$$0 = -\frac{dp}{dx} + \mu \frac{\partial^2 u}{\partial y^2}$$

Film fluide mince

$$h \ll L$$

Hypothèse de lubrification :
Écoulements rampants

$$\underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

Est-ce que l'hypothèse de lubrification est réaliste ?

$$L = 10 \text{ cm}$$

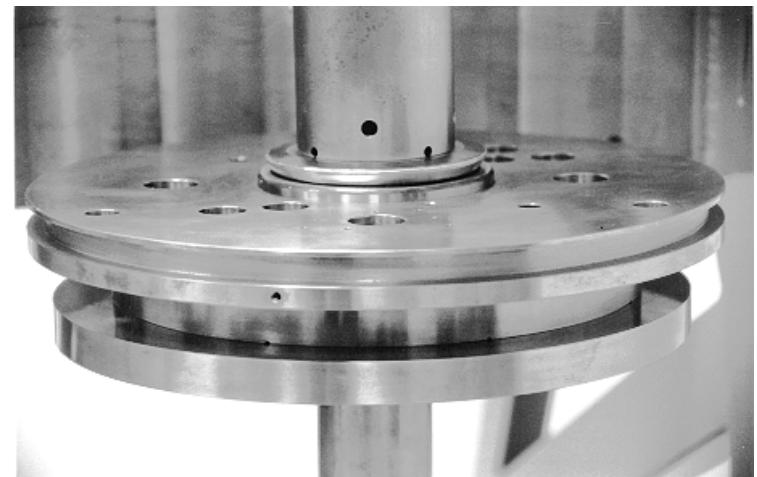
$$h = 0.5 \text{ mm}$$

$$U = 1 \text{ m/s}$$

$$\rho = 900 \text{ kg/m}^3$$
$$\mu = 60 \cdot 10^{-3} \text{ Ns/m}^2$$

Huile SAE50 à 60 degrés

$$\frac{\rho U L}{\underbrace{\mu}_{Re_L}} \frac{h^2}{L^2} \stackrel{0.0375}{\ll} 1$$



Huile SAE 50

C'est quoi ?

Transport maritime

Marine LCX

Une huile formulée spécialement pour la lubrification des gros moteurs diesel marins à crosse. Elle lubrifie les cylindres grâce à un indice de basicité très élevé de 70 et un grade SAE* 50.

Grades offerts :

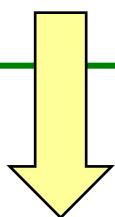
SAE 50

[Fiche technique](#)

[Fiche signalétique](#)

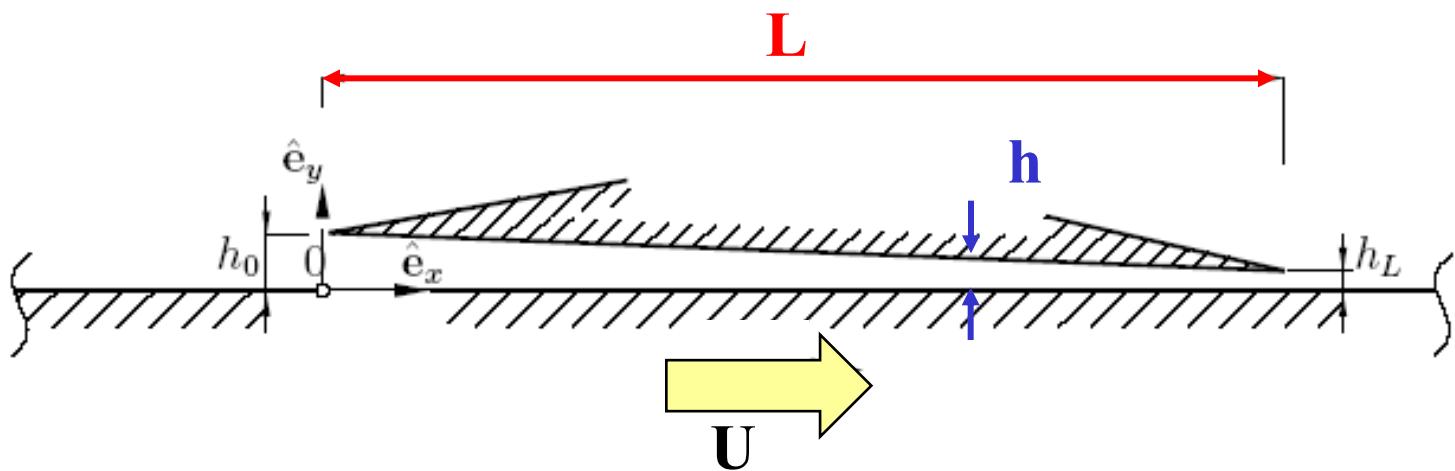
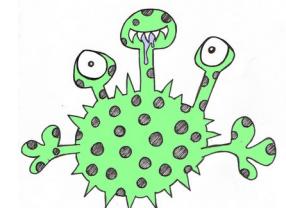


$$\left\{ \begin{array}{l} \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \\ -\frac{dp}{dx} + \mu \frac{\partial^2 u}{\partial y^2} = 0 \end{array} \right.$$



-i- calcul
de $u(x,y)$

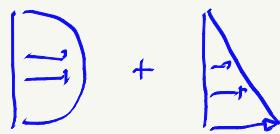
$$u(x, y) = -\frac{dp}{dx} \frac{h^2}{2\mu} \frac{y}{h} \left(1 - \frac{y}{h}\right) + U \left(1 - \frac{y}{h}\right)$$



5

**CALCUL
DU PROFIL
DE VITESSE :-)**

$$\frac{dp}{dx} = \mu \frac{\partial^2 v}{\partial y^2}$$



$$v(x, y) = - \underbrace{\frac{dp}{dx}}_{\left[\frac{N}{m^3} \right]} \underbrace{\frac{h^2}{2\mu} \left(1 - \frac{y}{h} \right) \frac{u}{h}}_{\left[\frac{m^2}{Ns} \right]} + U \left(1 - \frac{y}{h} \right)$$


$$\underbrace{\left[\frac{N}{m^3} \right]}_{\left[\frac{m}{s} \right]} \quad \underbrace{\left[\frac{m^2}{Ns} \right]}_{\left[\frac{1}{s} \right]}$$

$$\left[\frac{m}{s} \right] \rightarrow$$

$$\tau_z = 2\mu \frac{du}{dy}$$

$$\left[\frac{N}{m^2} \right] : \left[\frac{1}{s} \right]$$

$$\left[\frac{Ns}{m^2} \right]$$

6

CALCUL DE LA PRESSION

$$\frac{\partial v}{\partial x} + \frac{\partial r}{\partial y} = 0$$

$$0 = \int_0^h \frac{\partial v}{\partial x} dy + \int_0^h \frac{\partial r}{\partial y} dy$$

$$= \frac{d}{dx} \left[\int_0^h v dy \right]_0^h + [r]_0^h = 0$$

$\&(x)$

$$v(x, y) = - \frac{dp}{dx} \frac{h^2}{2M} \left(1 - \frac{y}{h}\right) \frac{u}{h} + U \left(1 - \frac{y}{h}\right)$$

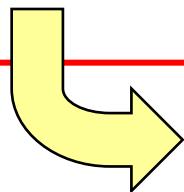


$$0 = \frac{d}{dx} \left[- \frac{dp(x)}{dx} \frac{h^2(x)}{2M} \int_0^h \left(1 - \frac{y}{h}\right) \frac{u}{h} dy + Uh \right]$$

$\frac{h}{6}$

$$\left\{ \begin{array}{l} -\frac{dp}{dx} + \mu \frac{\partial^2 u}{\partial y^2} = 0 \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \end{array} \right.$$

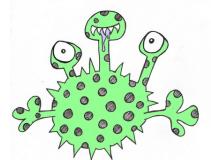
-ii- calcul
de $p(x)$



$$0 = \int_0^h \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} dy$$

$$0 = \frac{d}{dx} \overbrace{\int_0^h u(x, y) dy}^{Q(x)} + \left[v(x, y) \right]_0^h$$

En utilisant l'expression de $u(x, y)$



Equation classique de
Reynolds (1889)

$$0 = \frac{d}{dx} \left(-\frac{dp}{dx} \frac{h^3}{12\mu} + \frac{Uh}{2} \right)$$

$$O = \frac{d}{dx} \left[-\frac{dp(x)}{dx} \frac{h^2(x)}{2\mu} \int_0^h \underbrace{\left(1 - \frac{y}{h}\right) \frac{u}{h}}_{h/6} dy + \frac{Uh}{2} \right]$$

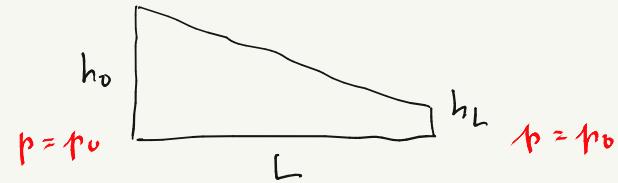
$$\frac{dh}{dx} = \frac{h_L - h_0}{L}$$

$$O = \frac{d}{dx} \left[-\frac{dp}{dx} \frac{h^3}{12\mu} + \frac{Uh}{2} \right]$$

$$\frac{d}{dx} \left[\frac{dp(x)}{dx} h^3(x) \right] = 6\mu U \frac{dh}{dx}$$

$$\left(\frac{dh}{dx}\right)^2 \frac{d}{dh} \left[\frac{dp}{dh} h^3 \right] = 6\mu U \frac{dh}{dx}$$

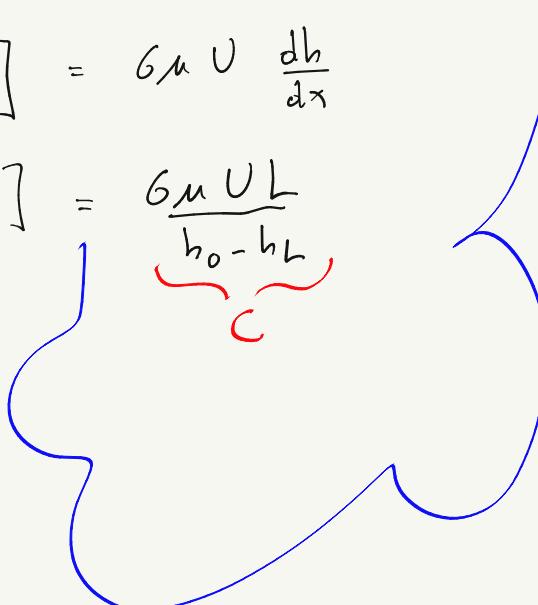
$$-\frac{d}{dh} \left[\frac{dp}{dh} h^3 \right] = \frac{6\mu U L}{h_0 - h_L}$$



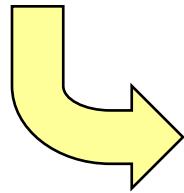
$$-\frac{dp}{dh} h^3 = C [h + A]$$

$$-\frac{dp}{dh} = C \left[\frac{1}{h^2} + \frac{A}{h^3} \right]$$

$$p(h) = C \left[\frac{1}{h} + \frac{A}{2h^2} + B \right]$$



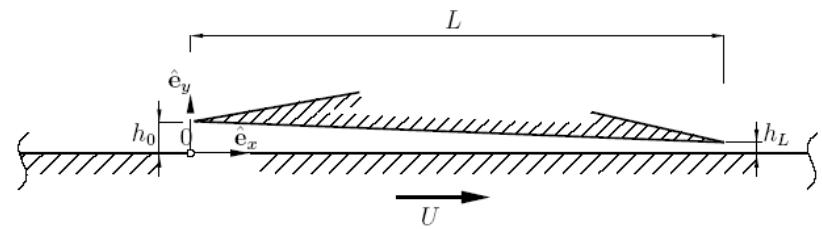
$$0 = \frac{d}{dx} \left(-\frac{dp}{dx} \frac{h^3}{12\mu} + \frac{Uh}{2} \right)$$



$$\frac{d}{dx} \left(h^3(x) \frac{dp}{dx}(x) \right) = 6\mu U \boxed{\frac{dh}{dx}}$$

$$-\frac{d}{dh} \left(h^3 \frac{dp}{dh}(h) \right) = \frac{6\mu UL}{h_0 - h_L}$$

Palier plat



$$\frac{x}{L} = \frac{h_0 - h(x)}{h_0 - h_L}$$

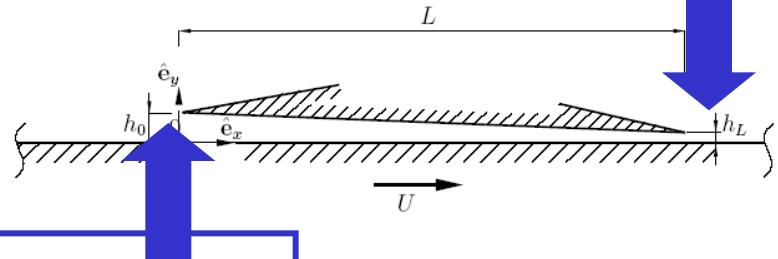
$$\frac{dh}{dx} = -\frac{h_0 - h_L}{L}$$

$$-h^3 \frac{dp}{dh}(h) = \frac{6\mu UL}{h_0 - h_L} (h + A)$$

$$-\frac{dp}{dh}(h) = \frac{6\mu UL}{h_0 - h_L} \left(\frac{1}{h^2} + \frac{A}{h^3} \right)$$

$$p(h) = \frac{6\mu UL}{h_0 - h_L} \left(B + \frac{1}{h} + \frac{A}{2h^2} \right)$$

$$p(h_L) = p_0$$



$$p(h_0) = p_0$$

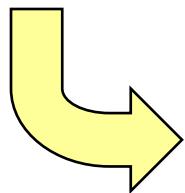
Deux conditions
aux limites

Deux
constantes

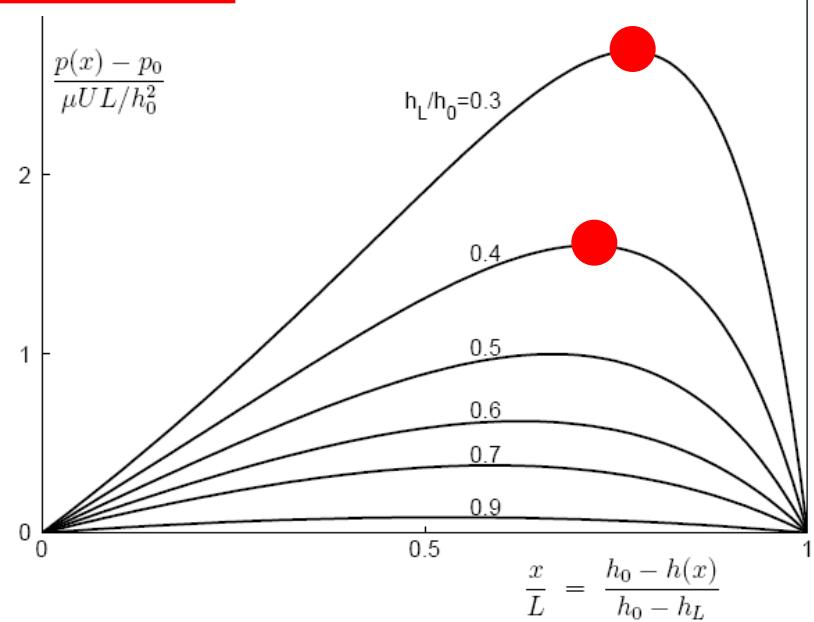
$$p(h) = \frac{6\mu UL}{h_0 - h_L} \left(B + \frac{1}{h} + \frac{A}{2h^2} \right)$$

$$p(h) - p_0 = \frac{6\mu UL(h_0 - h)(h - h_L)}{(h_0^2 - h_L^2)h^2}$$

Où la
pression
est-elle
maximale ?



$$h = \frac{2 h_0 h_L}{(h_0 + h_L)}$$

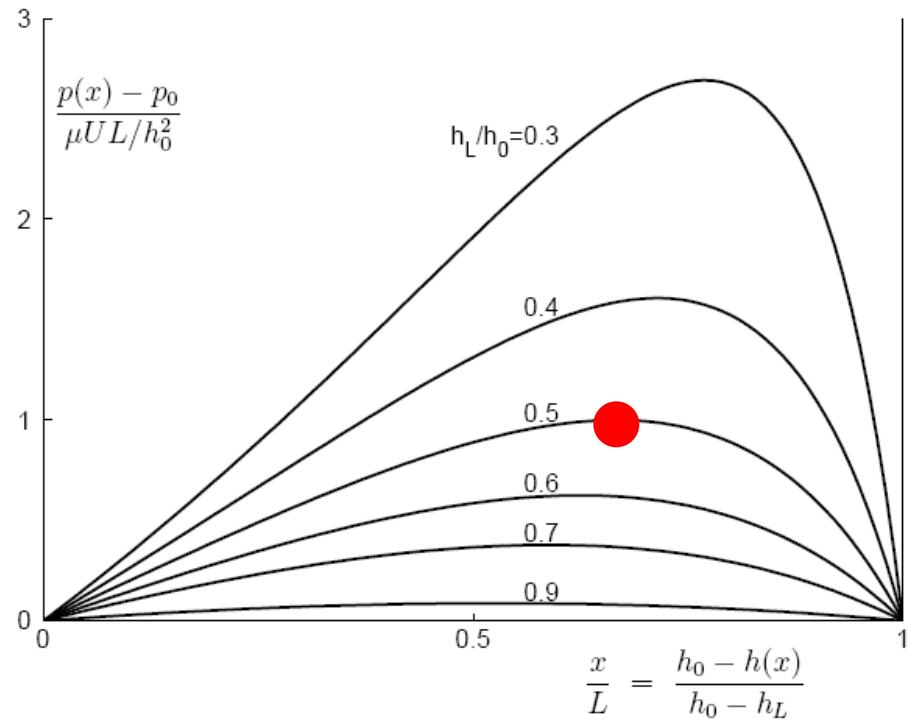


Cette pression
peut être
énorme !

$$\begin{aligned}L &= 10 \text{ cm} \\h_0 &= 0.1 \text{ mm} \\h_L &= 0.05 \text{ mm} \\U &= 10 \text{ m/s}\end{aligned}$$

$$\begin{aligned}\rho &= 900 \text{ kg/m}^3 \\ \mu &= 0.1 \text{ Ns/m}^2\end{aligned}$$

Huile SAE50 à 50 degrés



$$p_{\max} - p_0 = \frac{3 \mu U L}{2 h_0 h_L} \frac{(h_0 - h_L)}{(h_0 + h_L)}$$

10^7 Pascal

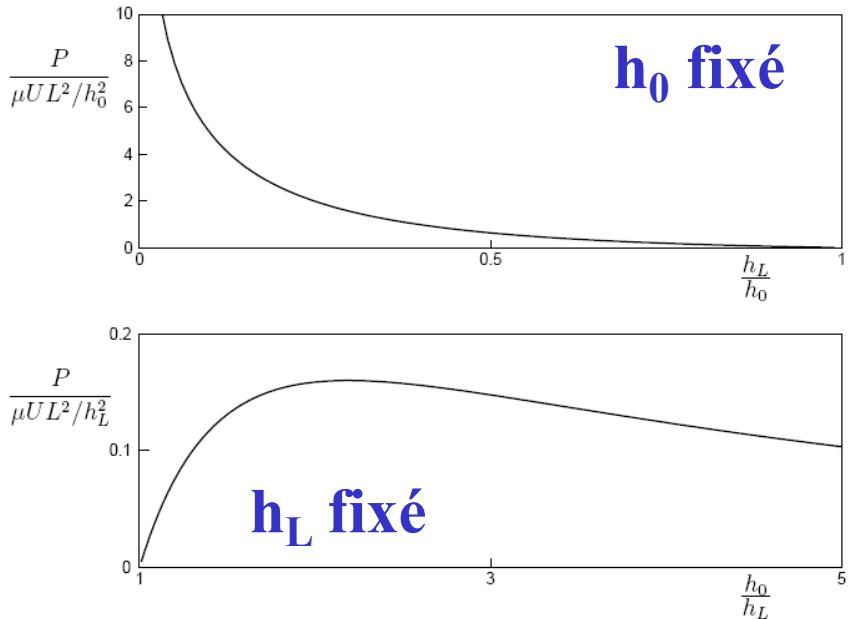
Charge utile

$$P = \int_0^L (p(x) - p_0) dx$$

$$= -\frac{L}{(h_0 - h_L)} \int_{h_0}^{h_L} (p(h) - p_0) dh$$

$$= -\frac{L}{(h_0 - h_L)} \frac{6 \mu U L}{(h_0^2 - h_L^2)} \int_{h_0}^{h_L} \left[(h_0 + h_L) \frac{1}{h} - \frac{h_0 h_L}{h^2} - 1 \right] dh$$

$$= -6 \mu U L^2 \left[\frac{1}{(h_0 - h_L)^2} \log \left(\frac{h_L}{h_0} \right) + \frac{2}{(h_0^2 - h_L^2)} \right]$$

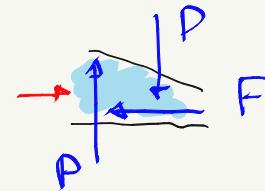
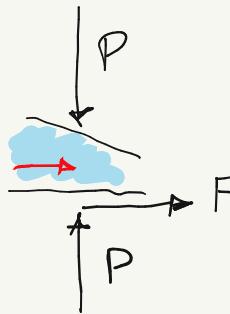
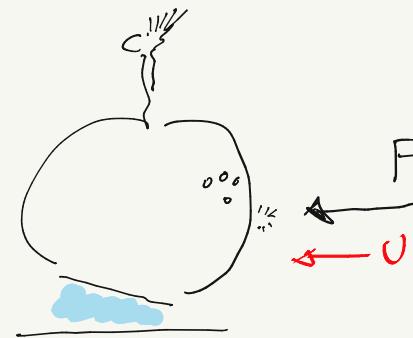


7

CHARGE

UTILE

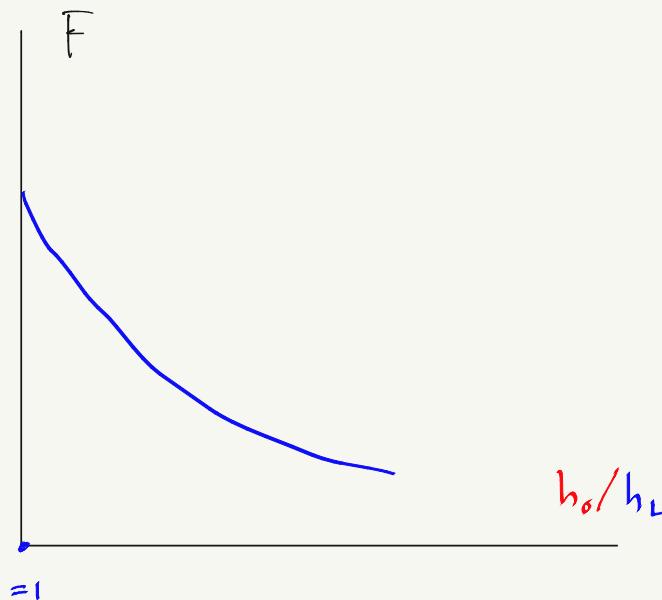
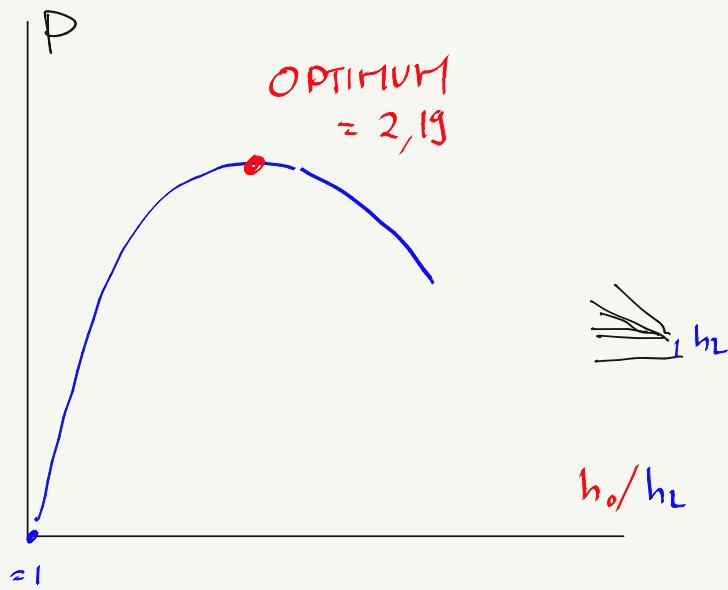
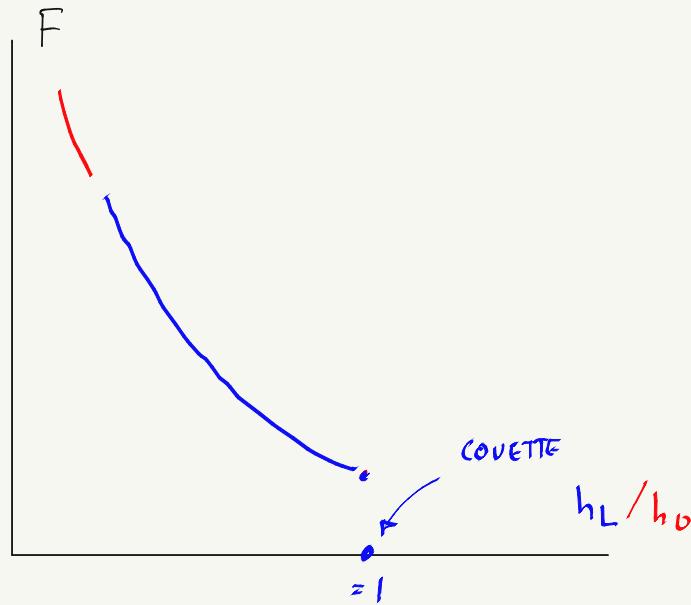
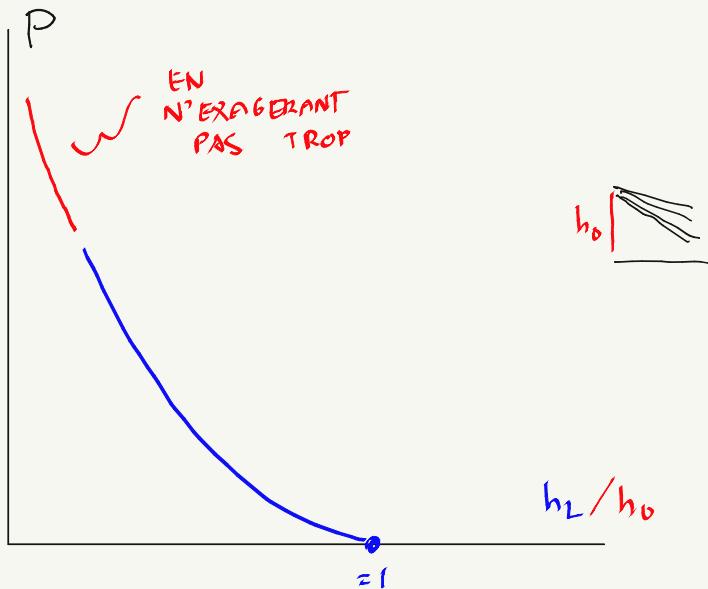
$$P = \int_0^L p(x) - p_0 \, dx$$

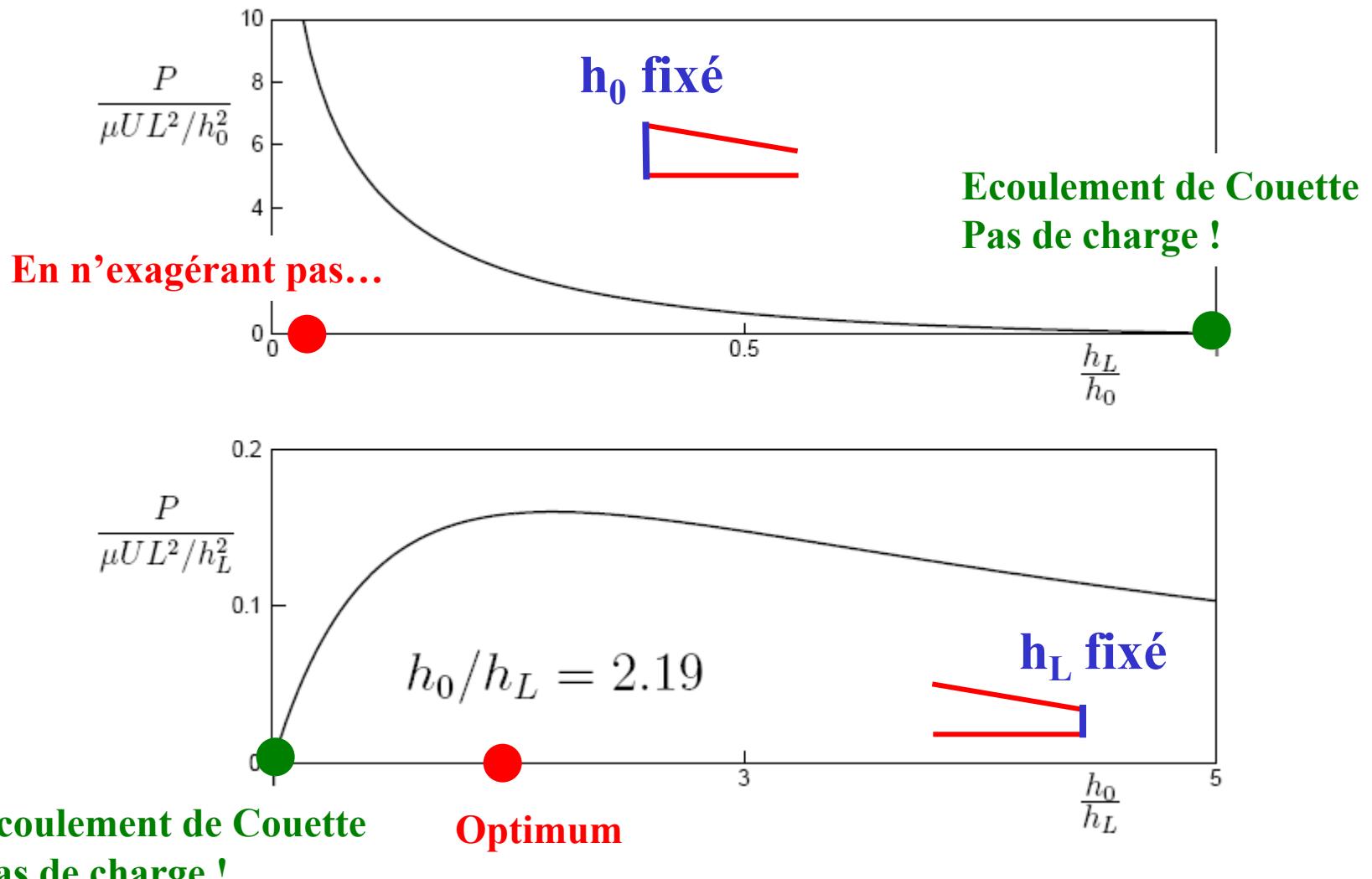
FORCE
DE POUSSÉE

$$F = -\mu \int_0^L \frac{\partial U}{\partial y} \, dx$$

PUISANCE
DISSIPÉE

FU :-)





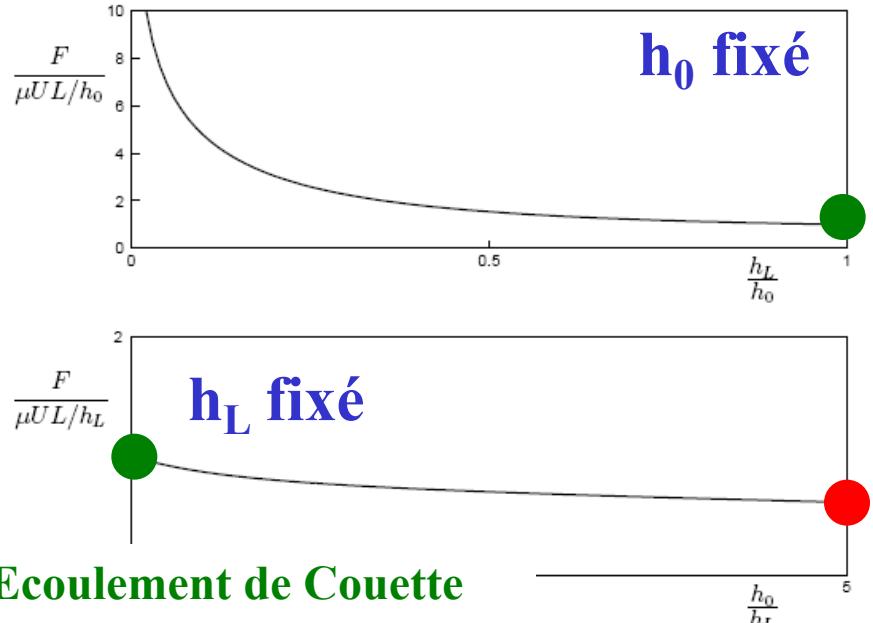
Rapport optimal...

Force exercée par le fluide sur la partie mobile

$$F = - \int_0^L \mu \frac{\partial u}{\partial y} \Big|_{y=0} dx$$

$$= \frac{\mu U L}{(h_0 - h_L)} \int_{h_0}^{h_L} \left[\frac{6}{h^2} \frac{h_0 h_L}{(h_0 + h_L)} - \frac{4}{h} \right] dh$$

$$= -\mu U L \left[\frac{6}{(h_0 + h_L)} + \frac{4}{(h_0 - h_L)} \log \left(\frac{h_L}{h_0} \right) \right]$$



Ecoulement de Couette
Pas de charge !

La force diminue de
façon monotone lorsque
le rapport augmente...

La puissance consommée est dissipée...

$$F U = -\frac{\mu U^2 L}{h_0} \left[\frac{6}{(1 + h_L/h_0)} + \frac{4}{(1 - h_L/h_0)} \log \left(\frac{h_L}{h_0} \right) \right]$$

Embêtant...

S'assurer que l'huile est bien refroidie car la viscosité (et donc la charge utile) décroît rapidement avec la température...

...en chaleur !

A propos de la viscosité de notre huile SAE 50

Transport maritime



Marine LCX

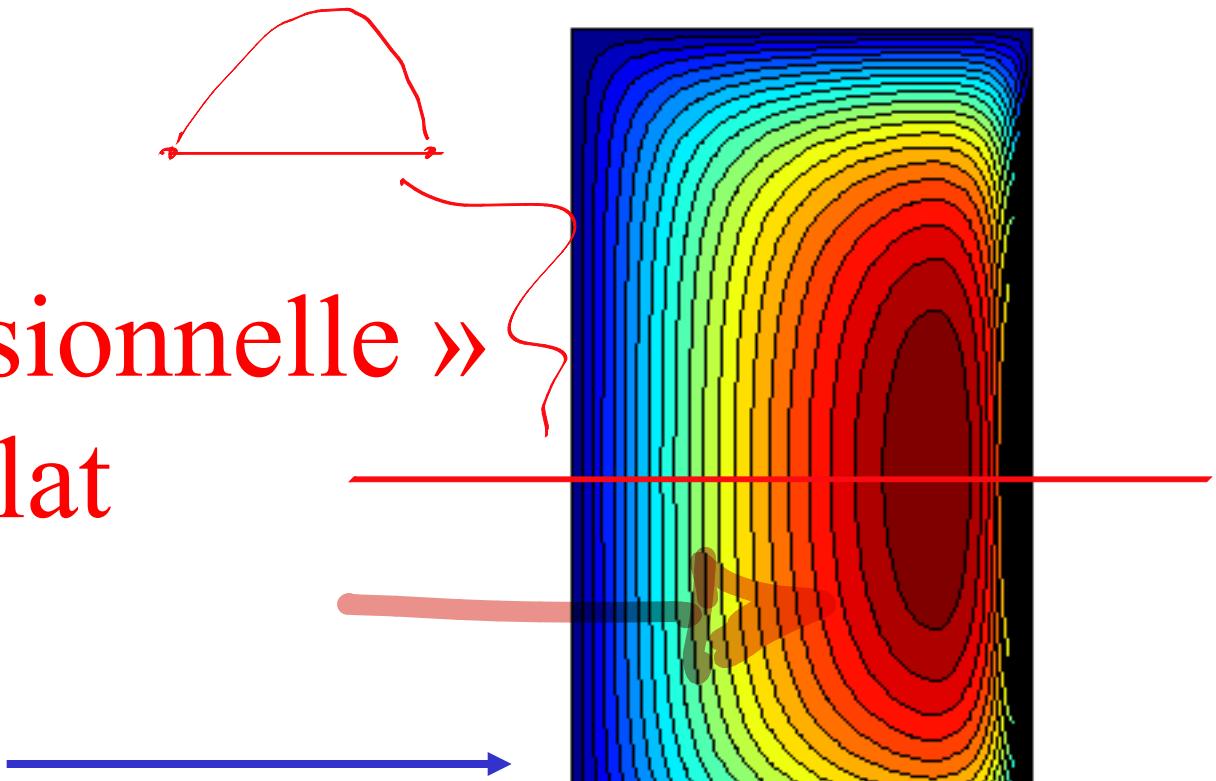
Une huile formulée spécialement pour la lubrification des gros moteurs diesel marins à crosse. Elle lubrifie les cylindres grâce à un indice de basicité très élevé de 70 et un grade SAE* 50.

Grades offerts :
SAE 50

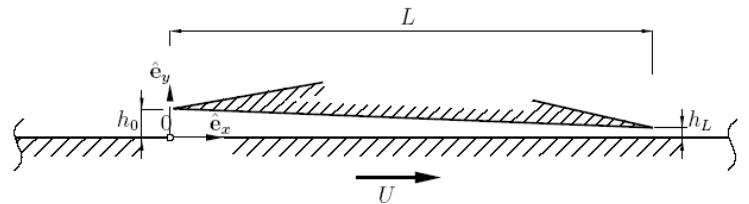
[Fiche technique](#)
[Fiche signalét](#)

$T = 20^{\circ}C$	$\mu = 1.100 \text{ Ns/m}^2$
$T = 40^{\circ}C$	$\mu = 0.210 \text{ Ns/m}^2$
$T = 50^{\circ}C$	$\mu = 0.100 \text{ Ns/m}^2$
$T = 60^{\circ}C$	$\mu = 0.060 \text{ Ns/m}^2$
$T = 80^{\circ}C$	$\mu = 0.025 \text{ Ns/m}^2$
$T = 100^{\circ}C$	$\mu = 0.013 \text{ Ns/m}^2$

Analyse « tridimensionnelle » du palier plat



pression sous un palier
dont la largeur vaut le
double de la longueur



Lubrification 2D 1/2

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

$$\frac{\partial p}{\partial x} = \mu \frac{\partial^2 u}{\partial z^2}$$

$$\frac{\partial p}{\partial y} = \mu \frac{\partial^2 v}{\partial z^2}$$

$$\frac{\partial p}{\partial z} = 0$$

Théorie de la
lubrification

Film fluide mince

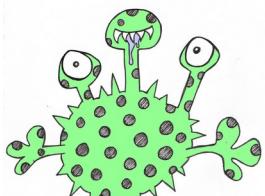
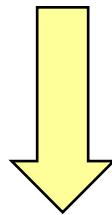
$$h \ll L$$

*Hypothèse de lubrification :
Écoulements rampants*

$$\underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

$$\left\{ \begin{array}{l} \boxed{\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0} \\ \\ \boxed{-\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial z^2} = 0} \\ \\ \boxed{-\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial z^2} = 0} \end{array} \right.$$

-i- calcul
de $u(x,y,z)$
et de $v(x,y,z)$

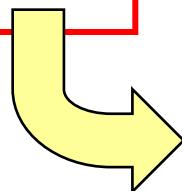


$$u(x, y, z) = -\frac{\partial p}{\partial x} \frac{h^2}{2\mu} \frac{z}{h} \left(1 - \frac{z}{h}\right) + U \left(1 - \frac{z}{h}\right)$$

$$v(x, y, z) = -\frac{\partial p}{\partial y} \frac{h^2}{2\mu} \frac{z}{h} \left(1 - \frac{z}{h}\right)$$

-ii- calcul de p(x,y)

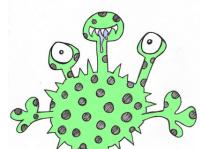
$$\left\{ \begin{array}{l} -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial z^2} = 0 \\ -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial z^2} = 0 \\ \hline \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \end{array} \right.$$



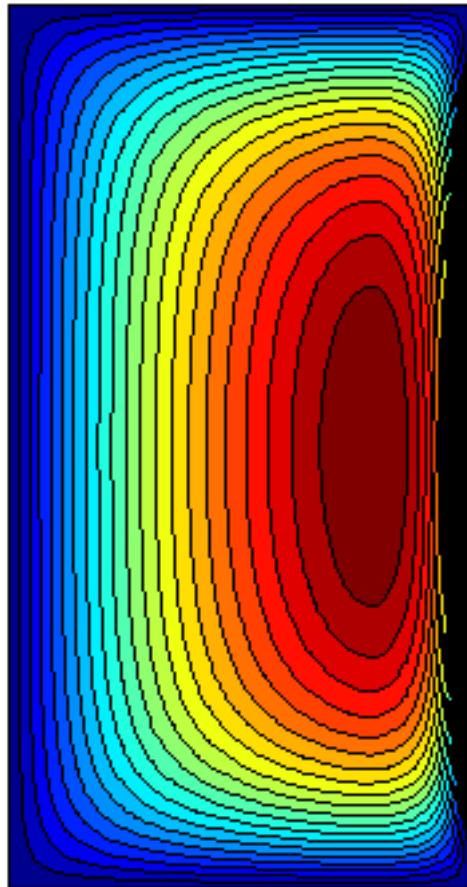
$$\int_0^h \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} dz = 0$$

$$\frac{\partial}{\partial x} \int_0^h u(x, y, z) dz + \frac{\partial}{\partial y} \int_0^h v(x, y, z) dz + \left[w(x, y, z) \right]_0^h = 0$$

~~w(x, y, z)~~



$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial p}{\partial x} \right) + \frac{\partial}{\partial y} \left(h^3 \frac{\partial p}{\partial y} \right) = 6\mu U \frac{dh}{dx}$$



-iiii- calcul
numérique par
différences finies
de $p(x,y)$

$$h^3 \left(\frac{\partial^2 p}{\partial x^2} + \frac{\partial^2 p}{\partial y^2} \right) + 3h^2 \left(\frac{h_L - h_0}{L} \right) \frac{\partial p}{\partial x} = 6\mu U \left(\frac{h_L - h_0}{L} \right)$$

TRANSPORT

DIFFUSION

