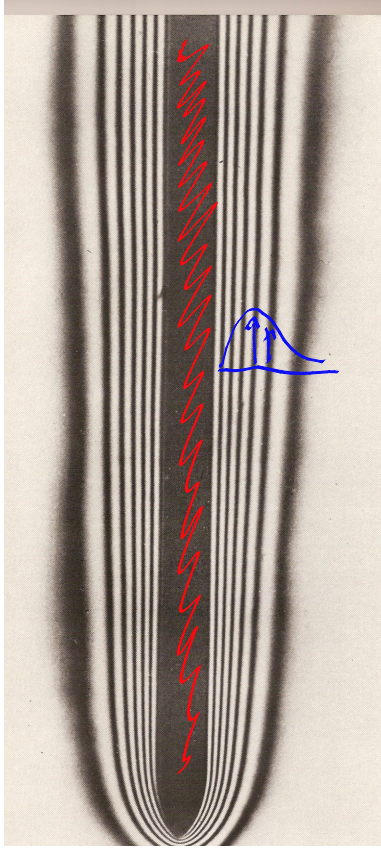


Mais que faire pour des écoulements avec deux échelles spatiales ?

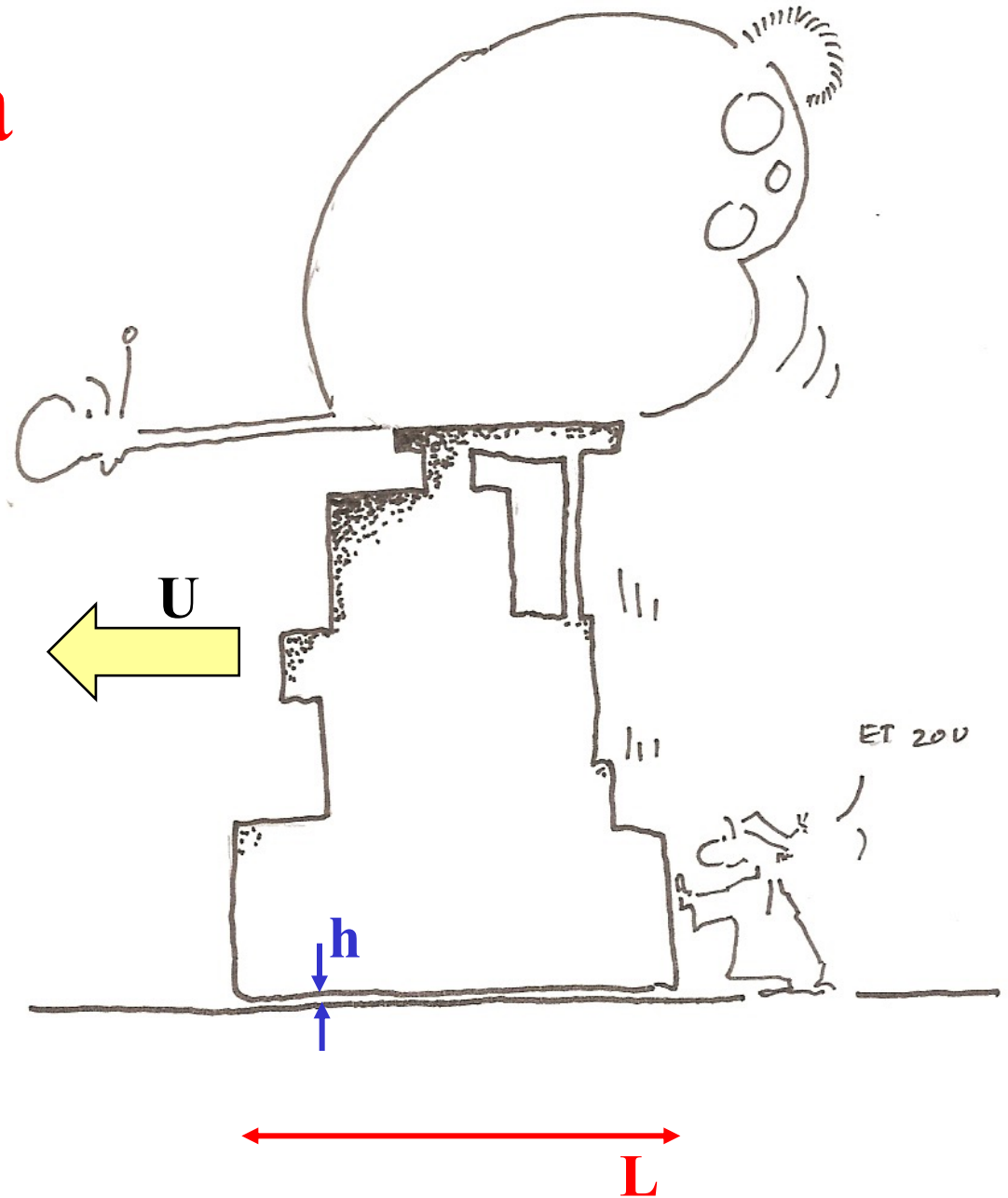


*Convection naturelle
le long d'une plaque
verticale : écoulement
laminaire permanent*



*Lubrification et convoyage
hydraulique : butée Michell*

Théorie de la lubrification

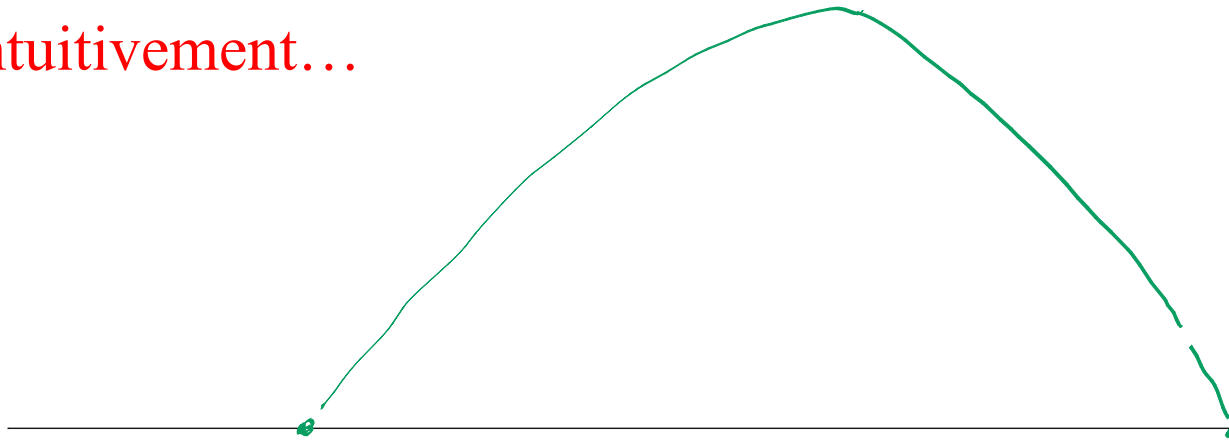


Convoyage hydraulique de charges très importantes :

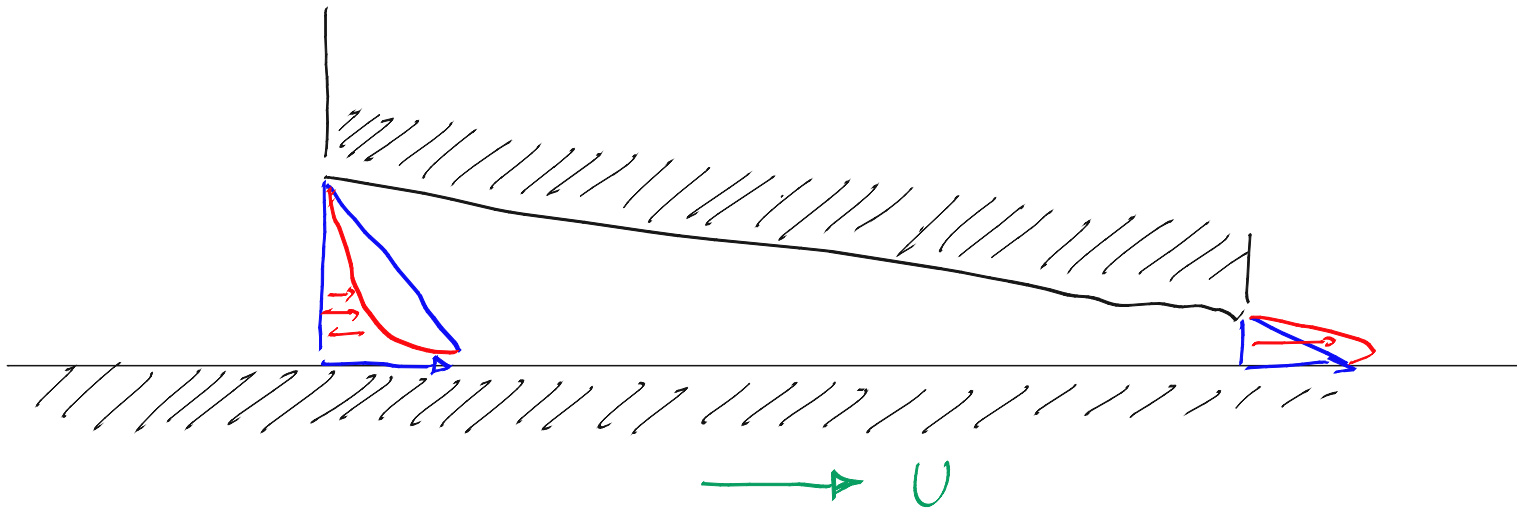
- turbines hydroélectriques
- applications marines
- butées hydrauliques

Intuitivement...

- ÉCOULEMENT STATIONNAIRE
INCOMPRESSIBLE
2D



MERCI
ANTOINE
D'INCOURT :-)

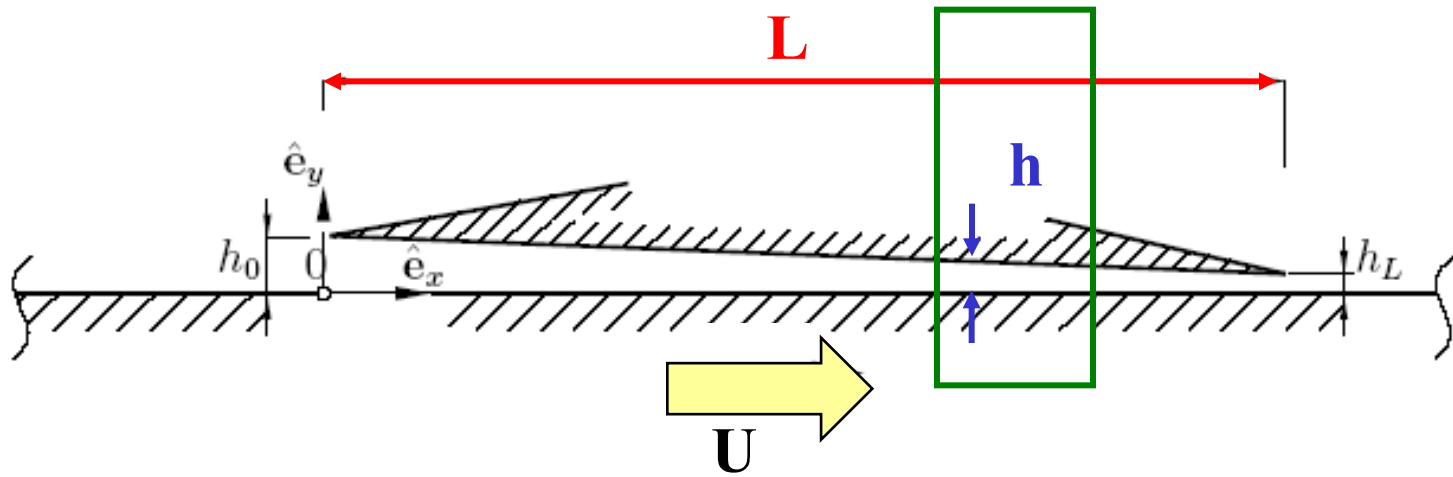
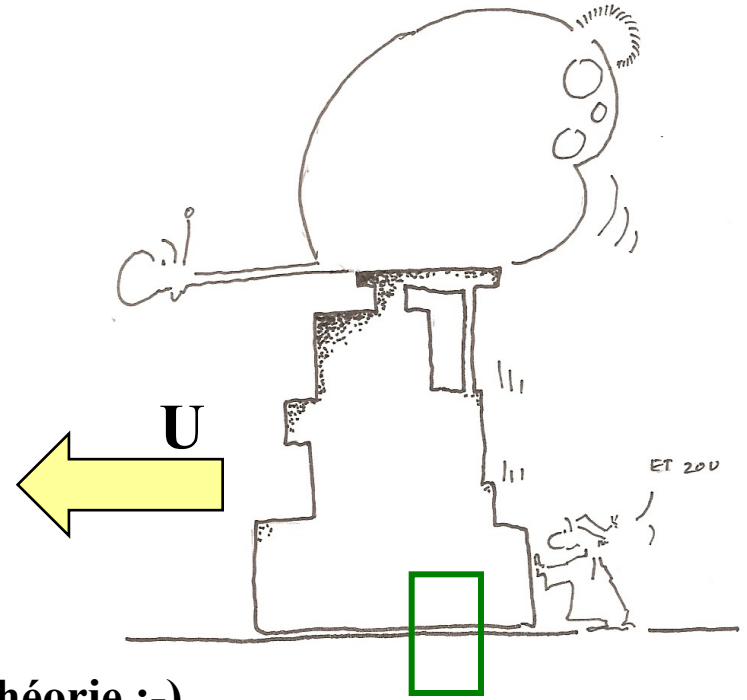


Théorie de la lubrification

$$h \ll L$$

Hypothèse géométrique de base

Valable dans la zone centrale uniquement en théorie :-)



Écoulements
incompressibles
plans
stationnaires

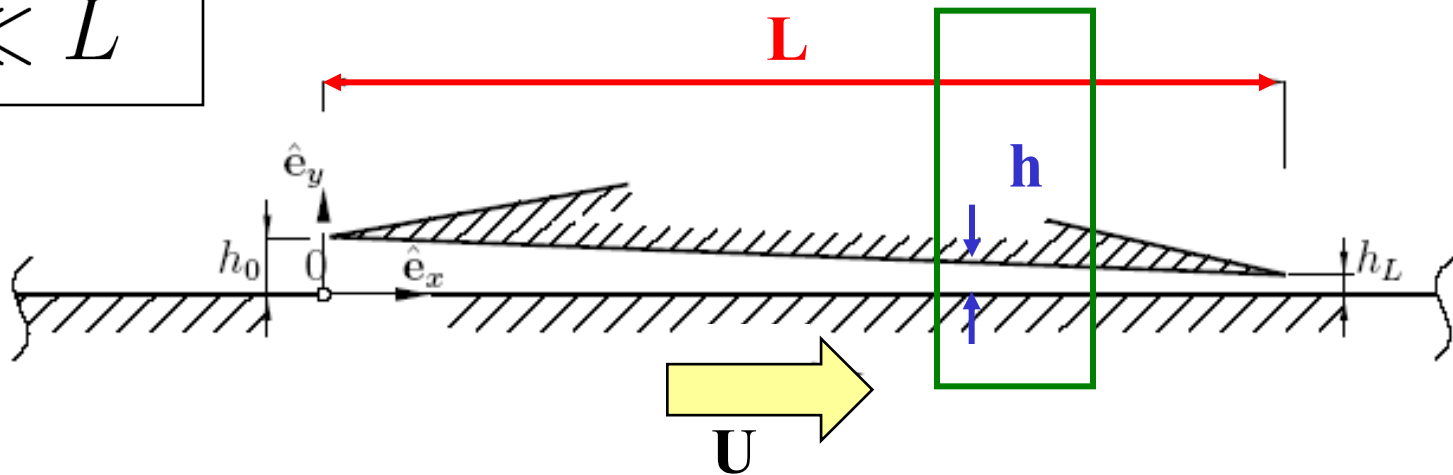
$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$\rho u \frac{\partial u}{\partial x} + \rho v \frac{\partial u}{\partial y} = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial x^2} + \mu \frac{\partial^2 u}{\partial y^2}$$

$$\rho u \frac{\partial v}{\partial x} + \rho v \frac{\partial v}{\partial y} = -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial x^2} + \mu \frac{\partial^2 v}{\partial y^2}$$

Que deviennent ces équations ?

$$h \ll L$$



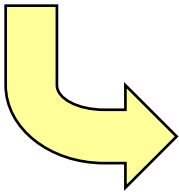
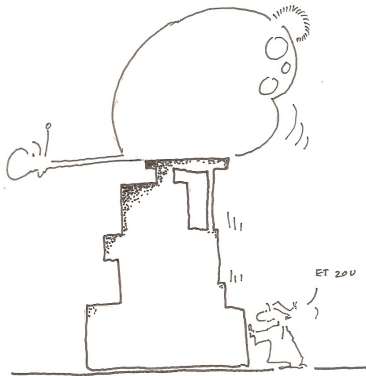
$$h \ll L$$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$
$$\rho u \frac{\partial u}{\partial x} + \rho v \frac{\partial u}{\partial y} = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial x^2} + \mu \frac{\partial^2 u}{\partial y^2}$$
$$\rho u \frac{\partial v}{\partial x} + \rho v \frac{\partial v}{\partial y} = -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial x^2} + \mu \frac{\partial^2 v}{\partial y^2}$$

Longueur horizontale caractéristique : L

Longueur verticale caractéristique : h

Vitesse horizontale caractéristique : U



**Comment choisir une
vitesse verticale
caractéristique ?**

Définir une vitesse
verticale caractéristique...

$$h \ll L$$

$$\frac{\partial \psi}{\partial x} + \frac{\partial \psi}{\partial y} = 0$$

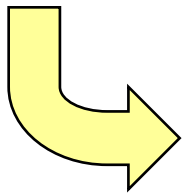


$$\frac{U}{L} \approx \frac{V}{h}$$

$$V \approx \frac{h}{L} U \ll U$$

$$\boxed{\mathcal{O}(U/L) \frac{\partial u}{\partial x}} + \boxed{\mathcal{O}(V/h) \frac{\partial v}{\partial y}} = 0$$

Il ne faut pas définir de vitesse caractéristique verticale !



$$V = \frac{Uh}{L} \ll U$$

Simplifions...

$$\underbrace{\cancel{\rho u \frac{\partial u}{\partial x}}}_{\cancel{\partial(\rho U^2/L)}} + \underbrace{\cancel{\rho v \frac{\partial u}{\partial y}}}_{\cancel{\partial(\rho V U/h)}} = - \frac{\partial p}{\partial x} + \underbrace{\cancel{\mu \frac{\partial^2 u}{\partial x^2}}}_{\cancel{\partial(\mu \frac{U}{L^2})}} + \underbrace{\mu \frac{\partial^2 u}{\partial y^2}}_{\partial(\mu \frac{U}{h^2})}$$

$$V = \frac{U h}{L}$$

$$\partial(\rho \frac{U h}{L} \frac{U}{h}) = \partial(\rho \frac{U^2}{L})$$

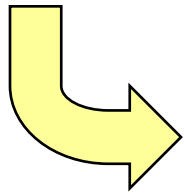
$$\frac{\text{INERTIE}}{\text{VISQUEUX}} = \frac{\rho U^2/L}{\mu U/h^2} = \underbrace{\frac{\rho U L}{\mu}}_{\text{Re}} \underbrace{\frac{h^2}{L^2}}_{\ll 1} \ll 1$$

EN SUPPOSANT
QUE Re RESTE
ACCEPTABLE

Quand peut-on négliger les termes d'inertie ?

$$\begin{array}{c} \mathcal{O}(\rho U^2/L) \\ \boxed{\rho u \frac{\partial u}{\partial x}} \end{array} + \begin{array}{c} \mathcal{O}(\rho U^2/L) \\ \boxed{\rho v \frac{\partial u}{\partial y}} \end{array} = -\frac{\partial p}{\partial x} + \begin{array}{c} \boxed{\mu \frac{\partial^2 u}{\partial x^2}} \end{array} + \begin{array}{c} \boxed{\mu \frac{\partial^2 u}{\partial y^2}} \end{array}$$

$\mathcal{O}(\rho VU/h) \qquad \mathcal{O}(\mu U/L^2) \ll \mathcal{O}(\mu U/h^2)$

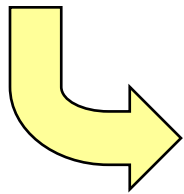


*Hypothèse de lubrification :
Écoulements rampants*

$$\frac{\boxed{\text{Forces d'inertie}}}{\boxed{\text{Forces visqueuses}}} = \frac{\rho U^2/L}{\mu U/h^2} = \underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

Et l'autre équation ?

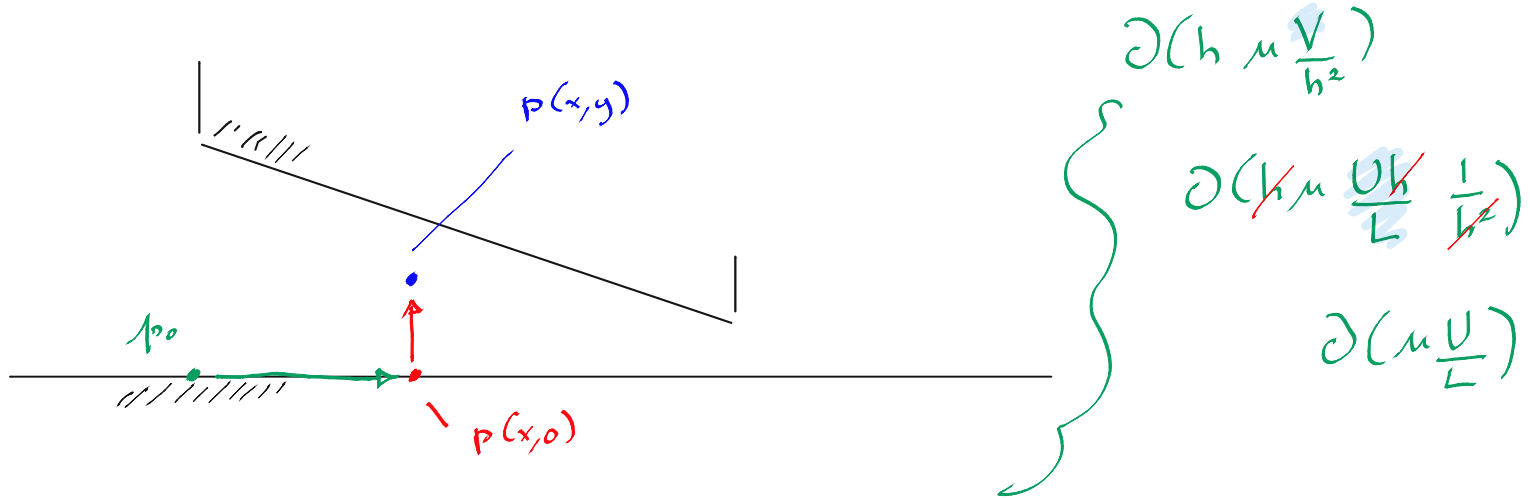
$$\begin{array}{c} \mathcal{O}(\rho U^2 h/L^2) \quad \mathcal{O}(\rho U^2 h/L^2) \\ \boxed{\cancel{\rho u \frac{\partial v}{\partial x}}} + \boxed{\cancel{\rho v \frac{\partial v}{\partial y}}} = -\frac{\partial p}{\partial y} + \boxed{\cancel{\mu \frac{\partial^2 v}{\partial x^2}}} + \boxed{\mu \frac{\partial^2 v}{\partial y^2}} \\ \mathcal{O}(\mu U h/L^3) \ll \mathcal{O}(\mu U/Lh) \end{array}$$



*On obtient la
même condition...*

$$\frac{\boxed{\text{Forces d'inertie}}}{\boxed{\text{Forces visqueuses}}} = \frac{\rho U^2 h/L^2}{\mu U/Lh} = \underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

Et la pression...



$$p(x,y) - p_0 = \boxed{p(x,0) - p_0} + \boxed{y \frac{\partial p}{\partial y} \Big|_{(x,0)}} + y^2 \dots$$

C'EST PETIT
CAR $y^2 \ll y \Rightarrow$

$\partial(L)$ \times $\frac{\partial p}{\partial x}$ \sim $\partial(\mu \frac{U}{h^2})$

$$\partial\left(\frac{\mu U}{L}\right)$$

$$p(x, y) - p_0 = \underbrace{p(x, 0) - p_0}_{\partial\left(\frac{\mu U L}{h^2}\right)} + \cancel{y \frac{\partial p}{\partial y} \Big|_{(x, 0)}} + \underbrace{y^2 \dots}_{\substack{\text{C'EST PETIT} \\ \text{CAR } y^2 \ll y \text{ :-)}}}$$

$$\frac{\mu U}{L} \frac{h^2}{L} \ll \frac{\mu U L}{h^2} \frac{h^2}{L}$$

$$\frac{h^2}{L^2} \mu U \ll \mu U$$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$0 = -\frac{dp}{dx} + \mu \frac{\partial^2 u}{\partial y^2}$$

Théorie de la lubrification

$$\boxed{\cancel{\rho u \frac{\partial v}{\partial x}}} + \boxed{\cancel{\rho v \frac{\partial v}{\partial y}}} = -\frac{\partial p}{\partial y} + \boxed{\cancel{\mu \frac{\partial^2 v}{\partial x^2}}} + \boxed{\mu \frac{\partial^2 v}{\partial y^2}}$$

$\mathcal{O}(\mu U/Lh)$

Et la pression ?

$$p(x, y) - p_0 = \boxed{p(x, 0) - p_0} + \boxed{y \cancel{\frac{\partial p}{\partial y}} \Big|_{y=0}}$$

$\mathcal{O}(\mu UL/h^2) \gg \mathcal{O}(\mu UL/L^2)$

$$\boxed{\cancel{\rho u \frac{\partial u}{\partial x}}} + \boxed{\cancel{\rho v \frac{\partial u}{\partial y}}} = -\frac{\partial p}{\partial x} + \boxed{\cancel{\mu \frac{\partial^2 u}{\partial x^2}}} + \boxed{\mu \frac{\partial^2 u}{\partial y^2}}$$

$\mathcal{O}(\mu U/h^2)$

Equations de Reynolds (1889)

Théorie de la
lubrification

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$0 = -\frac{dp}{dx} + \mu \frac{\partial^2 u}{\partial y^2}$$

Film fluide mince

$$h \ll L$$

*Hypothèse de lubrification :
Écoulements rampants*

$$\underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

Est-ce que l'hypothèse de lubrification est réaliste ?

$$\begin{aligned}L &= 10 \text{ cm} \\h &= 0.5 \text{ mm} \\U &= 1 \text{ m/s}\end{aligned}$$

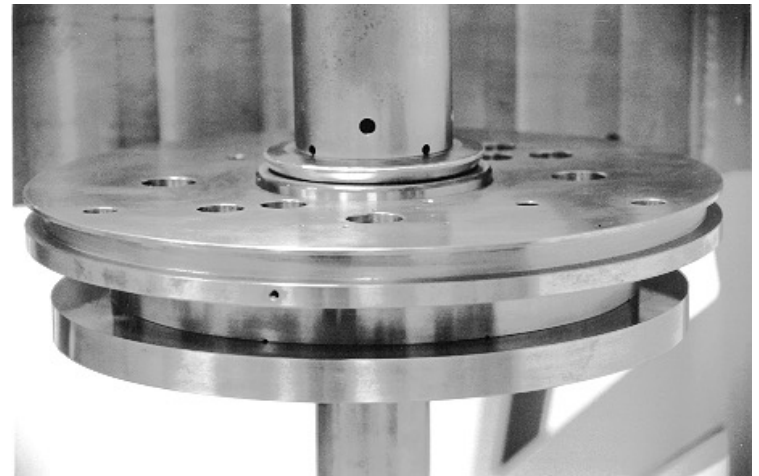
$$\begin{aligned}\rho &= 900 \text{ kg/m}^3 \\ \mu &= 60 \cdot 10^{-3} \text{ Ns/m}^2\end{aligned}$$

Huile SAE50 à 60 degrés

$$\frac{\rho U L}{\mu} \frac{h^2}{L^2} \ll 1$$

0.0375

Re_L



Huile SAE 50

C'est quoi ?

Transport maritime



Marine LCX

Une huile formulée spécialement pour la lubrification des gros moteurs diesel marins à crosse. Elle lubrifie les cylindres grâce à un indice de basicité très élevé de 70 et un grade SAE* 50.

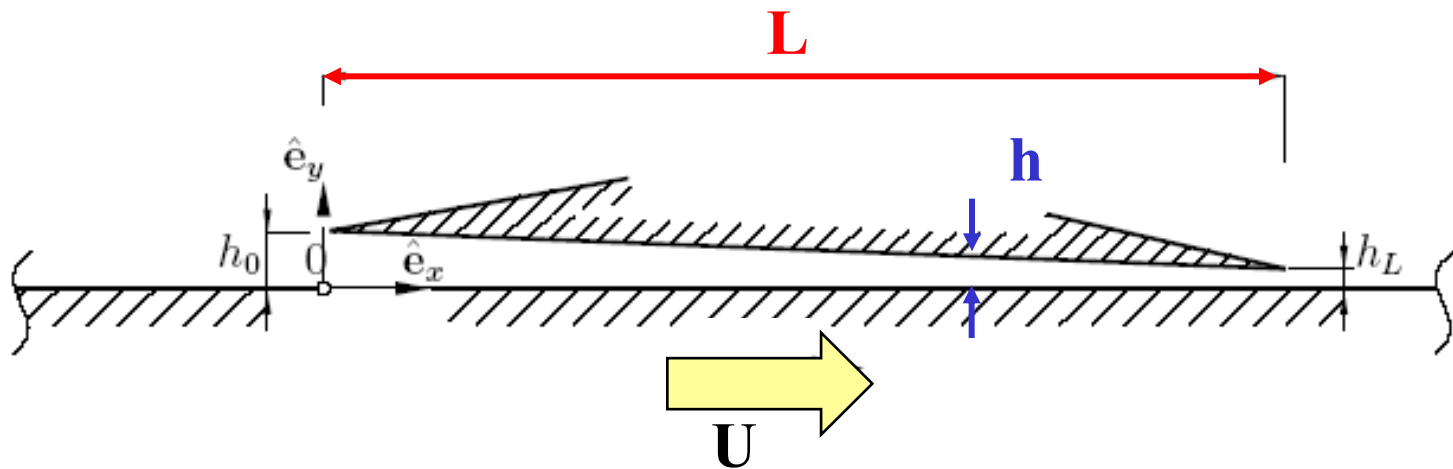
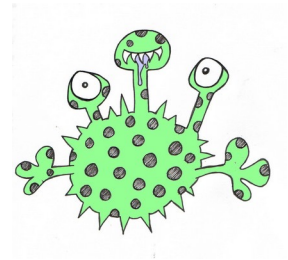
Grades offerts :
SAE 50

[Fiche technique](#)
[Fiche signalétique](#)

$$\left\{ \begin{array}{l} \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \\ -\frac{dp}{dx} + \mu \frac{\partial^2 u}{\partial y^2} = 0 \end{array} \right.$$

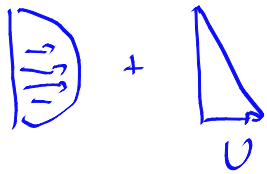
-i- calcul
de $u(x,y)$

$$u(x,y) = -\frac{dp}{dx} \frac{h^2}{2\mu} \frac{y}{h} \left(1 - \frac{y}{h}\right) + U \left(1 - \frac{y}{h}\right)$$



Calcul du profil de vitesse...

$$\frac{dp}{dx} = \mu \frac{\partial^2 u}{\partial y^2}$$



$$u(x, y) = - \underbrace{\frac{dp}{dx}}_{\text{force}} \underbrace{\frac{h^2}{2\mu}}_{\text{viscosity}} \left(1 - \frac{y}{h}\right) \frac{y}{h} + U \left(1 - \frac{y}{h}\right)$$

The equation is enclosed in a blue box. The terms $\frac{dp}{dx}$ and $\frac{h^2}{2\mu}$ are underlined with red brackets. To the right of the equation is a small drawing of a piston in a cylinder with a velocity vector U .

$$\underbrace{\left[\frac{N}{m^3} \right]}_{\left[\frac{m}{s} \right]} \underbrace{\left[\frac{m^2}{N \cdot s} \right]}_{\left[\frac{m}{s} \right]}$$

$$\tau = 2\mu \frac{du}{dy}$$


$$\left[\frac{N}{m^2} \right] \quad \left[\frac{1}{s} \right]$$

Calcul du profil de pression...

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$0 = \int_0^h \frac{\partial u}{\partial x} dy + \int_0^h \frac{\partial v}{\partial y} dy$$

$$= \frac{d}{dx} \underbrace{\int_0^h u dy}_{Q(x)} + \underbrace{[v]_0^h}_{=0}$$

$$u(x, y) = -\frac{dp}{dx} \frac{h^2}{2\mu} \left(1 - \frac{y}{h}\right) \frac{y}{h} + U \left(1 - \frac{y}{h}\right)$$


$$0 = \frac{d}{dx} \left[-\frac{dp}{dx}(x) \frac{h^2(x)}{2\mu} \underbrace{\int_0^{h(x)} \left(1 - \frac{y}{h}\right) \frac{y}{h} dy}_{\frac{h(x)}{6}} + U \frac{h}{2} \right]$$

$$0 = \frac{d}{dx} \left[-\frac{dp}{dx}(x) \frac{h^2(x)}{2\mu} \int_0^{h(x)} \underbrace{\left(1 - \frac{y}{h}\right) \frac{y}{h}}_{\frac{h(x)}{6}} dy + U \frac{h}{2} \right]$$

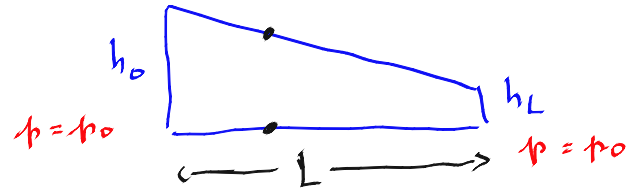
$$0 = \frac{d}{dx} \left[-\frac{dp}{dx} \frac{h^3}{12\mu} + \frac{Uh}{2} \right]$$

$$\frac{d}{dx} \left[\frac{dp}{dx}(x) h^3(x) \right] = 6\mu U \frac{dh}{dx}$$

$$\left(\frac{dh}{dx}\right)^2 \frac{d}{dh} \left[\frac{dp}{dh} h^3 \right] = 6\mu U \frac{dh}{dx}$$

$$-\frac{d}{dh} \left[\frac{dp}{dh} h^3 \right] = \underbrace{\frac{6\mu U L}{h_0 - h_L}}_C$$

$$\frac{dh}{dx} = \frac{h_L - h_0}{L}$$

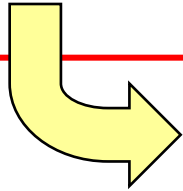


$$-\frac{dp}{dh} h^3 = C [h + A]$$

$$-\frac{dp}{dh} = C \left[\frac{1}{h^2} + \frac{A}{h^3} \right]$$

$$p(h) = C \left[\frac{1}{h} + \frac{A}{2h^2} + B \right]$$

$$\begin{cases} -\frac{dp}{dx} + \mu \frac{\partial^2 u}{\partial y^2} = 0 \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \end{cases}$$

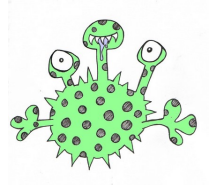


**-ii- calcul
de p(x)**

$$0 = \int_0^h \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} dy$$

$$0 = \frac{d}{dx} \overbrace{\int_0^h u(x, y) dy}^{Q(x)} + \cancel{\left[v(x, y) \right]_0^h}$$

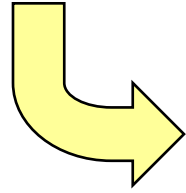
En utilisant l'expression de u(x,y)



**Equation classique de
Reynolds (1889)**

$$0 = \frac{d}{dx} \left(-\frac{dp}{dx} \frac{h^3}{12\mu} + \frac{Uh}{2} \right)$$

$$0 = \frac{d}{dx} \left(-\frac{dp}{dx} \frac{h^3}{12\mu} + \frac{Uh}{2} \right)$$



$$\frac{d}{dx} \left(h^3(x) \frac{dp}{dx}(x) \right) = 6\mu U \frac{dh}{dx}$$

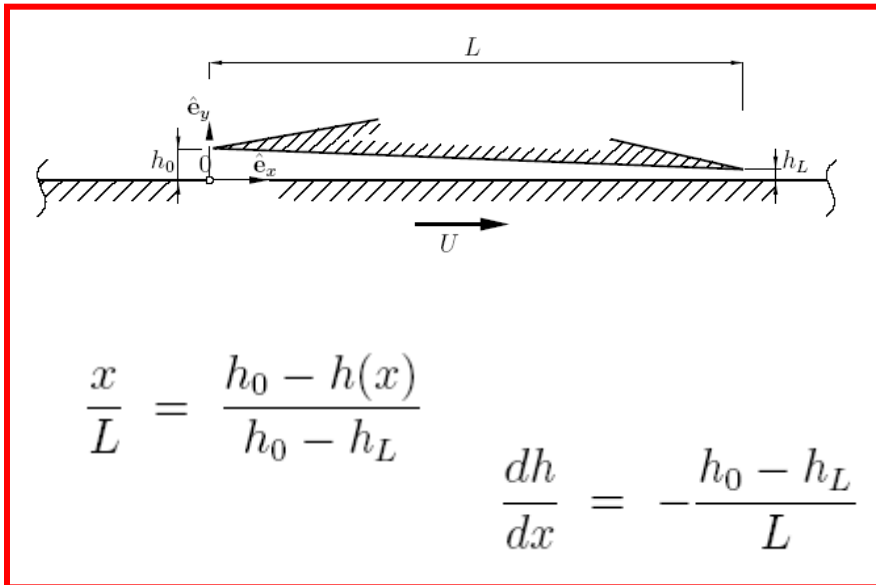
$$-\frac{d}{dh} \left(h^3 \frac{dp}{dh}(h) \right) = \frac{6\mu UL}{h_0 - h_L}$$

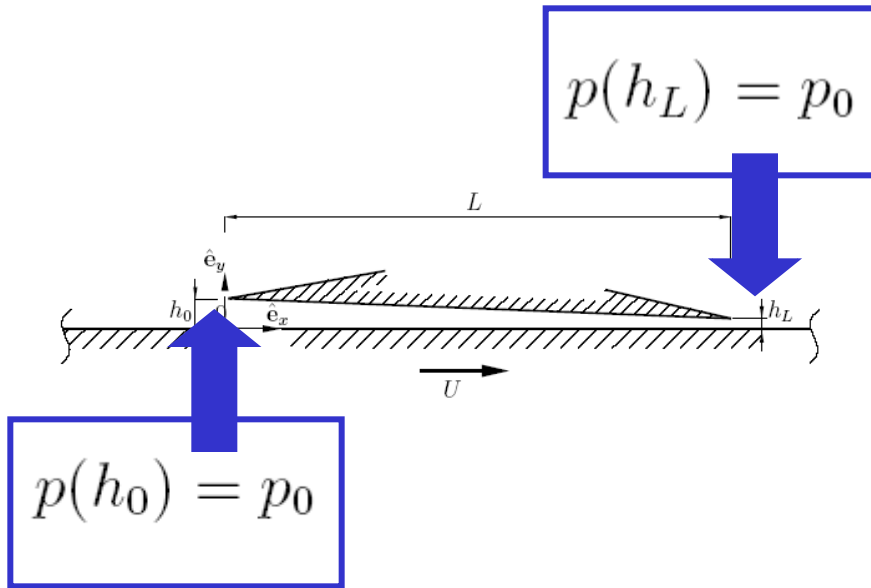
$$-h^3 \frac{dp}{dh}(h) = \frac{6\mu UL}{h_0 - h_L} (h + A)$$

$$-\frac{dp}{dh}(h) = \frac{6\mu UL}{h_0 - h_L} \left(\frac{1}{h^2} + \frac{A}{h^3} \right)$$

~~$$p(h) = \frac{6\mu UL}{h_0 - h_L} \left(B + \frac{1}{h} + \frac{A}{2h^2} \right)$$~~

Palier plat





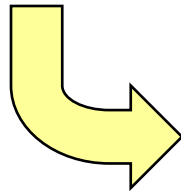
Deux conditions
aux limites

Deux
constantes

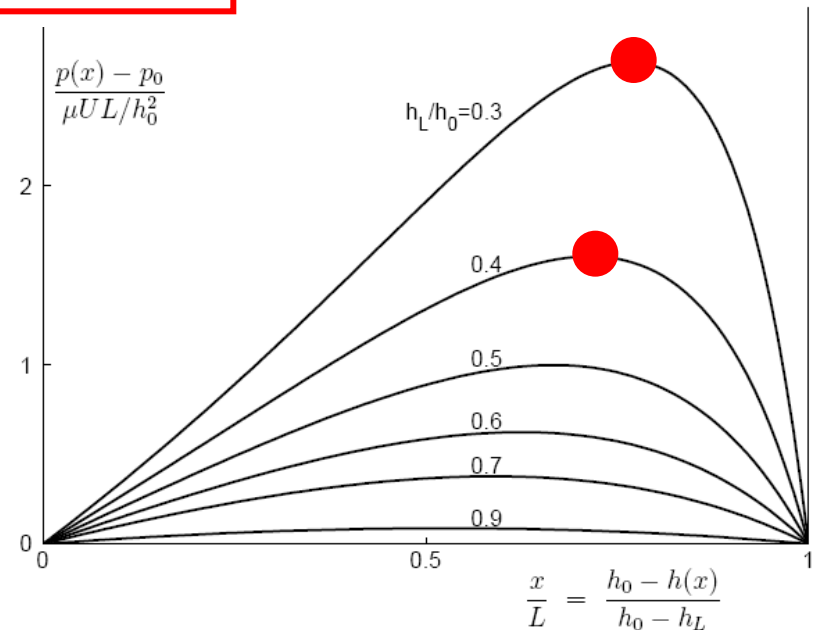
$$p(h) = \frac{6\mu UL}{h_0 - h_L} \left(\boxed{B} + \frac{1}{h} + \frac{\boxed{A}}{2h^2} \right)$$

$$p(h) - p_0 = \frac{6\mu UL(h_0 - h)(h - h_L)}{(h_0^2 - h_L^2)h^2}$$

Où la
pression
est-elle
maximale ?



$$h = \frac{2 h_0 h_L}{(h_0 + h_L)}$$

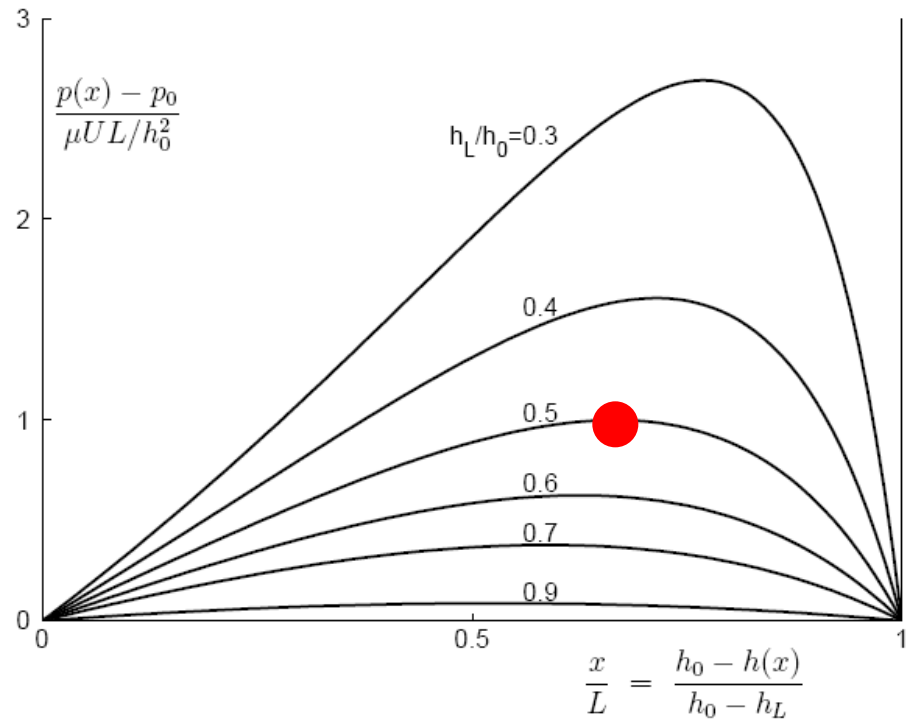


Cette pression
peut être
énorme !

$$\begin{aligned}L &= 10 \text{ cm} \\h_0 &= 0.1 \text{ mm} \\h_L &= 0.05 \text{ mm} \\U &= 10 \text{ m/s}\end{aligned}$$

$$\begin{aligned}\rho &= 900 \text{ kg/m}^3 \\ \mu &= 0.1 \text{ Ns/m}^2\end{aligned}$$

Huile SAE50 à 50 degrés

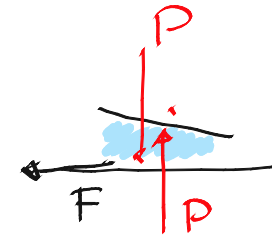
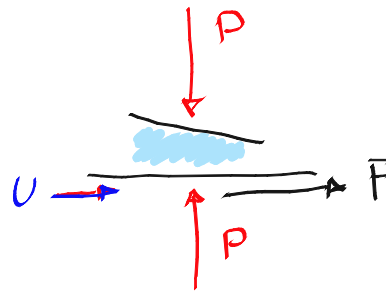
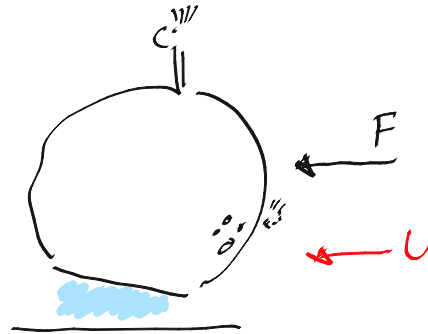


$$p_{\max} - p_0 = \frac{3 \mu U L (h_0 - h_L)}{2 h_0 h_L (h_0 + h_L)}$$

10^7 Pascal

Charge utile

$$P = \int_0^L p(x) - p_0 \, dx$$



$$F = -\mu \int_0^L \frac{\partial u}{\partial y} \, dx$$

Force de poussée

Puissance
dissipée

FU

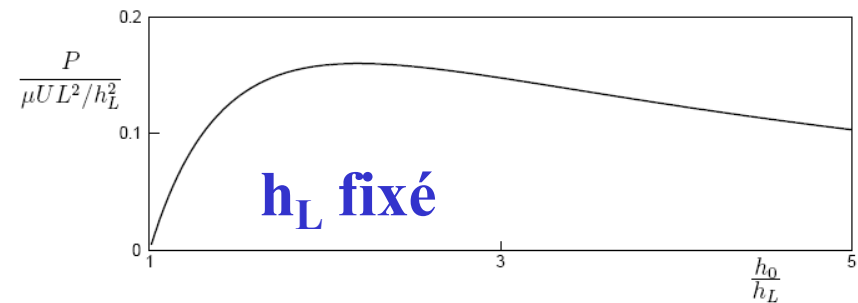
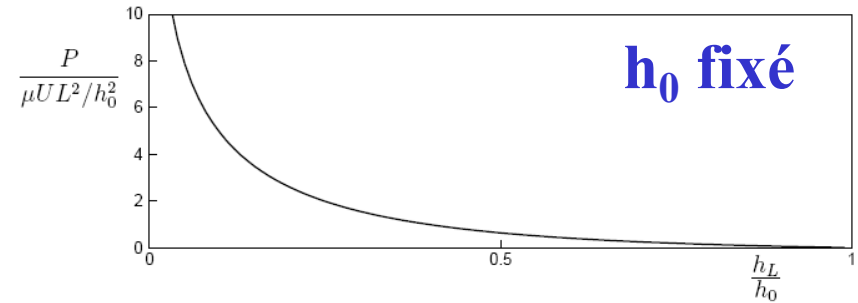
Charge utile

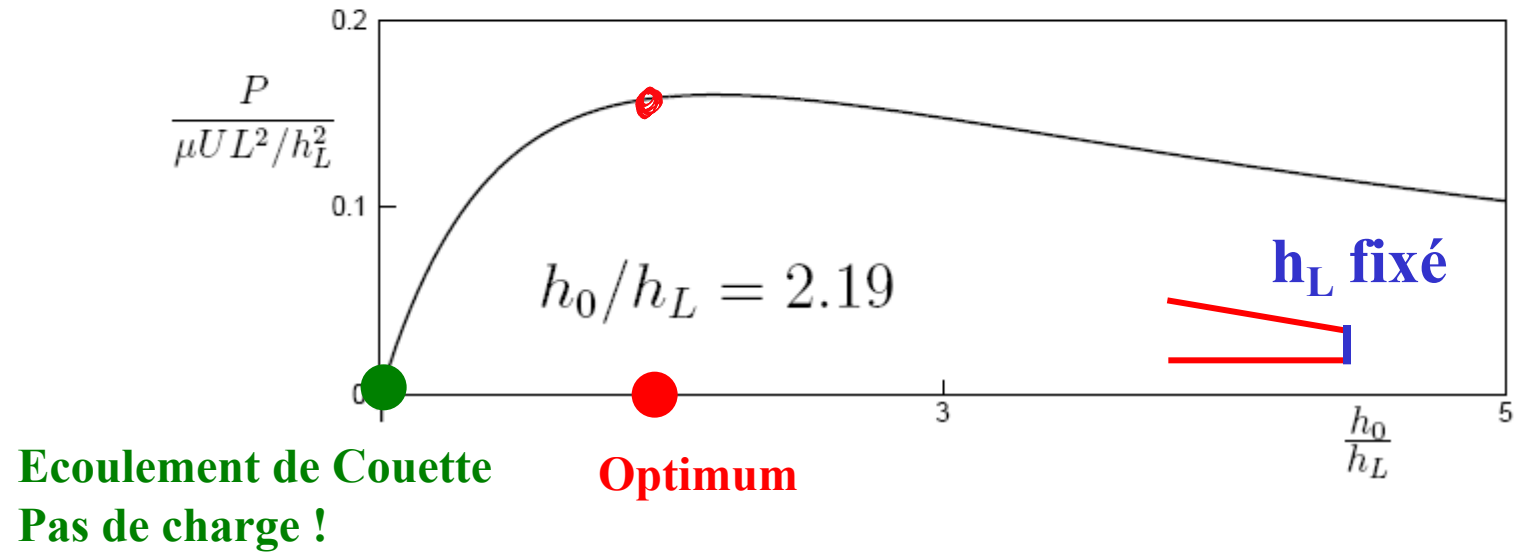
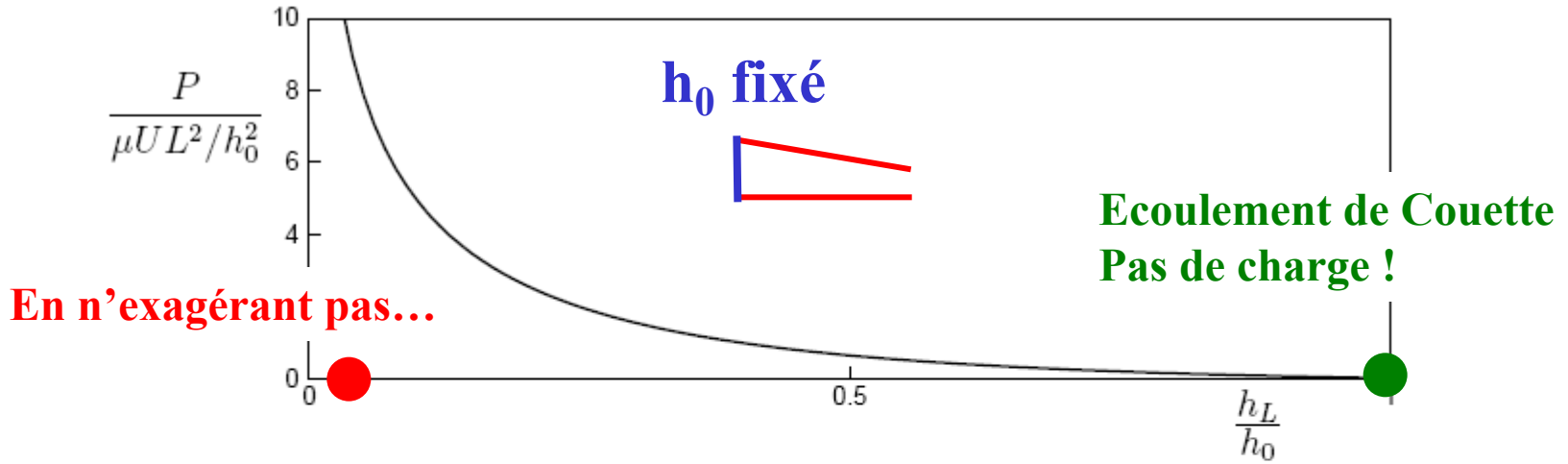
$$P = \int_0^L (p(x) - p_0) dx$$

$$= -\frac{L}{(h_0 - h_L)} \int_{h_0}^{h_L} (p(h) - p_0) dh$$

$$= -\frac{L}{(h_0 - h_L)} \frac{6 \mu U L}{(h_0^2 - h_L^2)} \int_{h_0}^{h_L} \left[(h_0 + h_L) \frac{1}{h} - \frac{h_0 h_L}{h^2} - 1 \right] dh$$

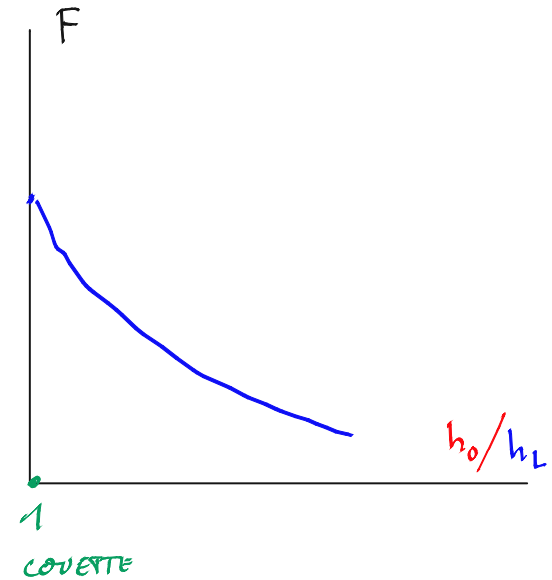
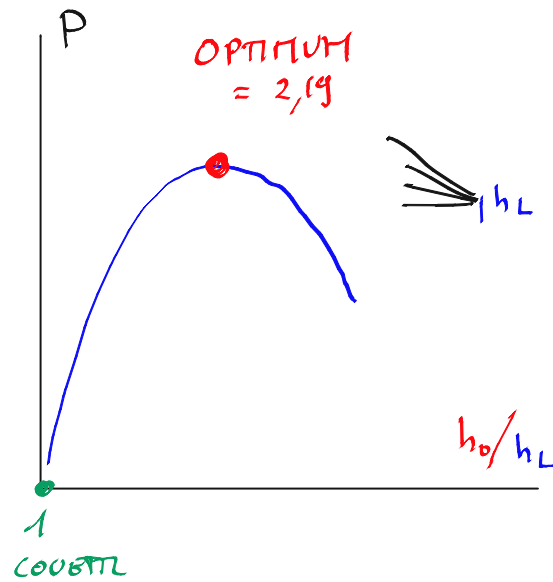
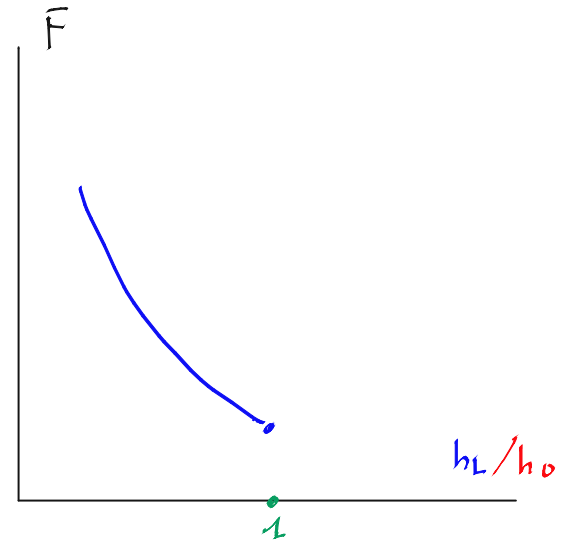
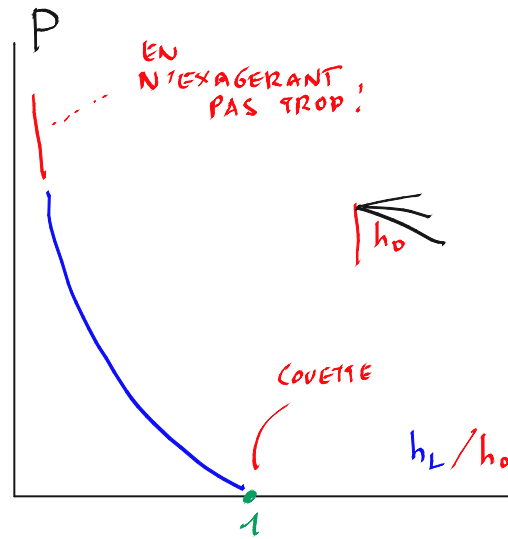
$$= -6 \mu U L^2 \left[\frac{1}{(h_0 - h_L)^2} \log \left(\frac{h_L}{h_0} \right) + \frac{2}{(h_0^2 - h_L^2)} \right]$$



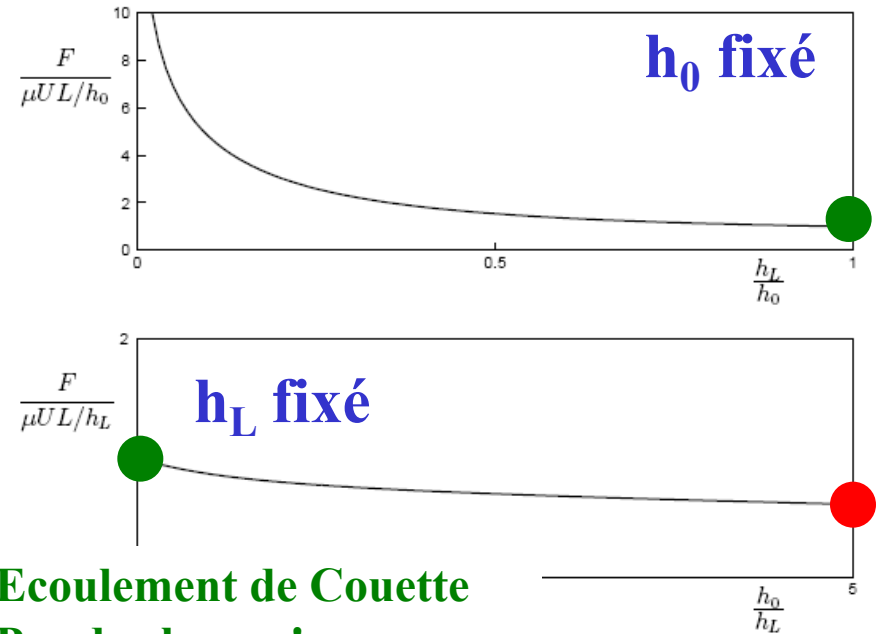


Rapport optimal...

Quatre petits graphes !



Force exercée par le fluide sur la partie mobile



Ecoulement de Couette
Pas de charge !

**La force diminue de
façon monotone lorsque
le rapport augmente...**

$$\begin{aligned}
 F &= - \int_0^L \mu \left. \frac{\partial u}{\partial y} \right|_{y=0} dx \\
 &= \frac{\mu U L}{(h_0 - h_L)} \int_{h_0}^{h_L} \left[\frac{6}{h^2} \frac{h_0 h_L}{(h_0 + h_L)} - \frac{4}{h} \right] dh \\
 &= -\mu U L \left[\frac{6}{(h_0 + h_L)} + \frac{4}{(h_0 - h_L)} \log \left(\frac{h_L}{h_0} \right) \right]
 \end{aligned}$$

La puissance consommée est dissipée...

$$F U = -\frac{\mu U^2 L}{h_0} \left[\frac{6}{(1 + h_L/h_0)} + \frac{4}{(1 - h_L/h_0)} \log \left(\frac{h_L}{h_0} \right) \right]$$

Embêtant...

S'assurer que l'huile est bien refroidie car la viscosité (et donc la charge utile) décroît rapidement avec la température...

...en chaleur !

A propos de la viscosité de notre huile SAE 50

Transport maritime



Marine LCX

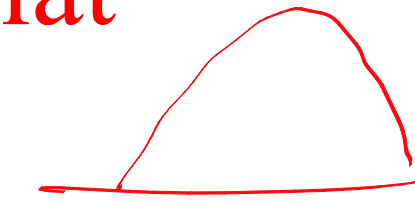
Une huile formulée spécialement pour la lubrification des gros moteurs diesel marins à crosse. Elle lubrifie les cylindres grâce à un indice de basicité très élevé de 70 et un grade SAE* 50.

Grades offerts :
SAE 50

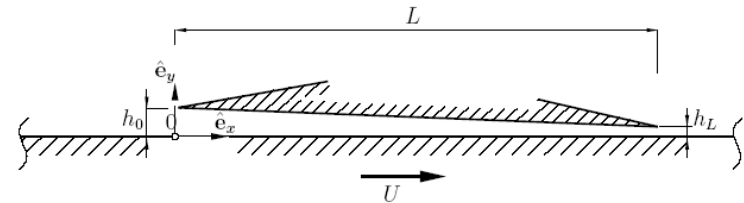
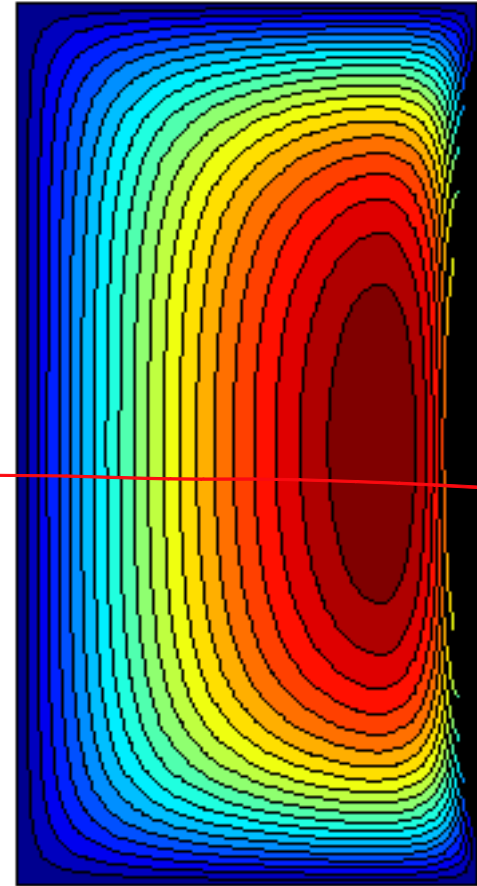
[Fiche technique](#)
[Fiche signalét](#)

$T = 20^{\circ}C$	$\mu = 1.100 \text{ N s/m}^2$
$T = 40^{\circ}C$	$\mu = 0.210 \text{ N s/m}^2$
$T = 50^{\circ}C$	$\mu = 0.100 \text{ N s/m}^2$
$T = 60^{\circ}C$	$\mu = 0.060 \text{ N s/m}^2$
$T = 80^{\circ}C$	$\mu = 0.025 \text{ N s/m}^2$
$T = 100^{\circ}C$	$\mu = 0.013 \text{ N s/m}^2$

Analyse « tridimensionnelle » du palier plat



pression sous un palier
dont la largeur vaut le
double de la longueur



Lubrification 2D $\frac{1}{2}$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

$$\frac{\partial p}{\partial x} = \mu \frac{\partial^2 u}{\partial z^2}$$

$$\frac{\partial p}{\partial y} = \mu \frac{\partial^2 v}{\partial z^2}$$

$$\frac{\partial p}{\partial z} = 0$$

Film fluide mince

$$h \ll L$$

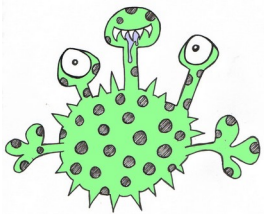
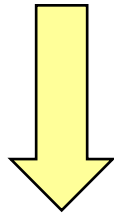
*Hypothèse de lubrification :
Écoulements rampants*

$$\underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

**Théorie de la
lubrification**

$$\left\{ \begin{array}{l} \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \\ -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial z^2} = 0 \\ -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial z^2} = 0 \end{array} \right.$$

-i- calcul
de $u(x,y,z)$
et de $v(x,y,z)$

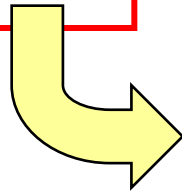


$$u(x, y, z) = -\frac{\partial p}{\partial x} \frac{h^2}{2\mu} \frac{z}{h} \left(1 - \frac{z}{h}\right) + U \left(1 - \frac{z}{h}\right)$$

$$v(x, y, z) = -\frac{\partial p}{\partial y} \frac{h^2}{2\mu} \frac{z}{h} \left(1 - \frac{z}{h}\right)$$

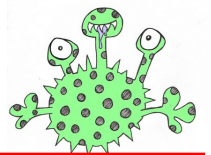
-ii- calcul
de $p(x,y)$

$$\begin{cases} -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial z^2} = 0 \\ -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial z^2} = 0 \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \end{cases}$$

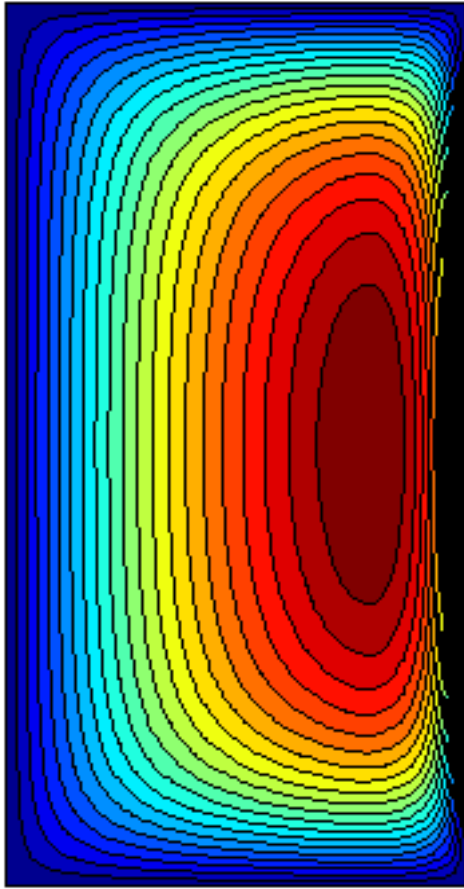


$$\int_0^h \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} dz = 0$$

$$\frac{\partial}{\partial x} \int_0^h u(x,y,z) dz + \frac{\partial}{\partial y} \int_0^h v(x,y,z) dz + \left[\cancel{w(x,y,z)} \right]_0^h = 0$$



$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial p}{\partial x} \right) + \frac{\partial}{\partial y} \left(h^3 \frac{\partial p}{\partial y} \right) = 6\mu U \frac{dh}{dx}$$




-iiii- calcul
numérique par
différences finies
de $p(x,y)$

$$h^3 \left(\frac{\partial^2 p}{\partial x^2} + \frac{\partial^2 p}{\partial y^2} \right) + 3h^2 \left(\frac{h_L - h_0}{L} \right) \frac{\partial p}{\partial x} = 6\mu U \left(\frac{h_L - h_0}{L} \right)$$

Un triple diplôme belgo-germano-français ?

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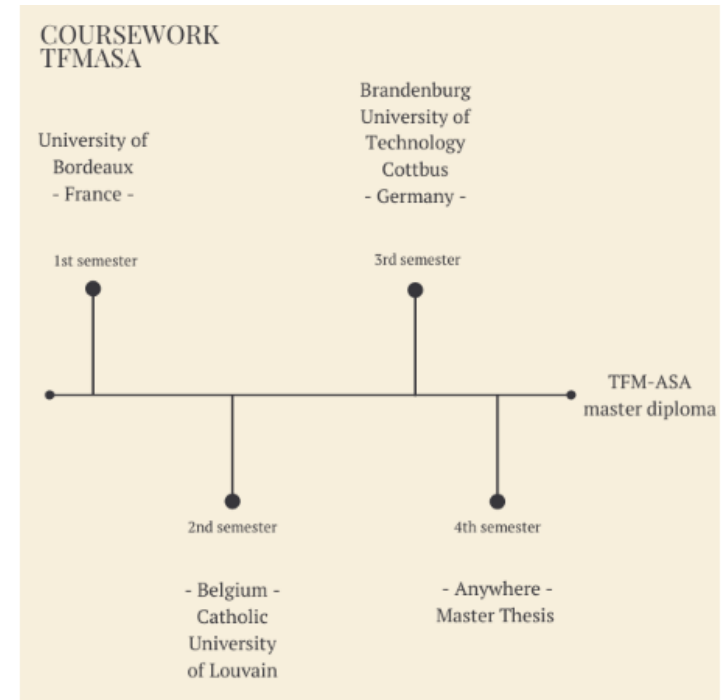
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en deux années !



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