C'est quoi physiquement le nombre de Reynolds ?

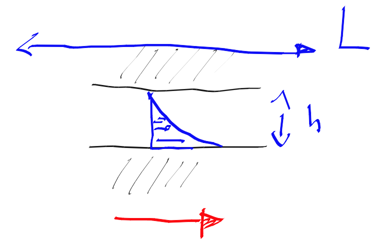
Effets visqueux
Diffusion de la quantité de mouvement

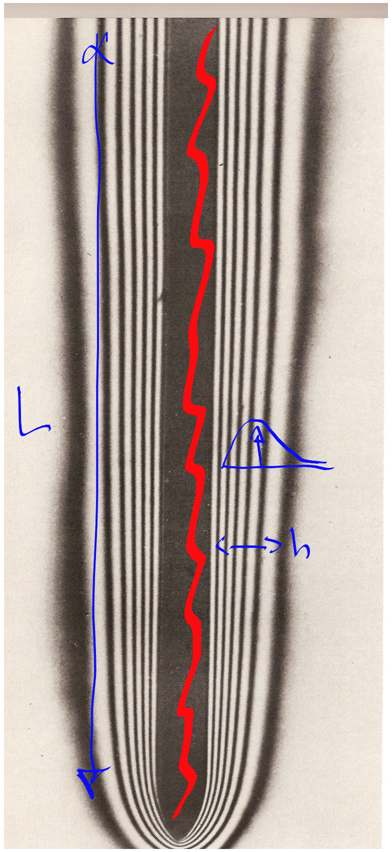
$$\boxed{\underset{\mathcal{O}(\rho U^2/L)}{\rho(\mathbf{v}\cdot\boldsymbol{\nabla})\mathbf{v}}} = -\boldsymbol{\nabla}p + \boxed{\underset{\mathcal{O}(\mu U/L^2)}{\mu\boldsymbol{\nabla}^2\mathbf{v}}}$$

Effets d'inertie
Transport de la quantité de mouvement

$$Re = \frac{\boxed{\text{Forces d'inertie}}}{\boxed{\text{Forces visqueuses}}} = \frac{\rho U^2/L}{\mu U/L^2} = \frac{\rho U L}{\mu}$$

Mais que faire pour des écoulements avec deux échelles spatiales ?

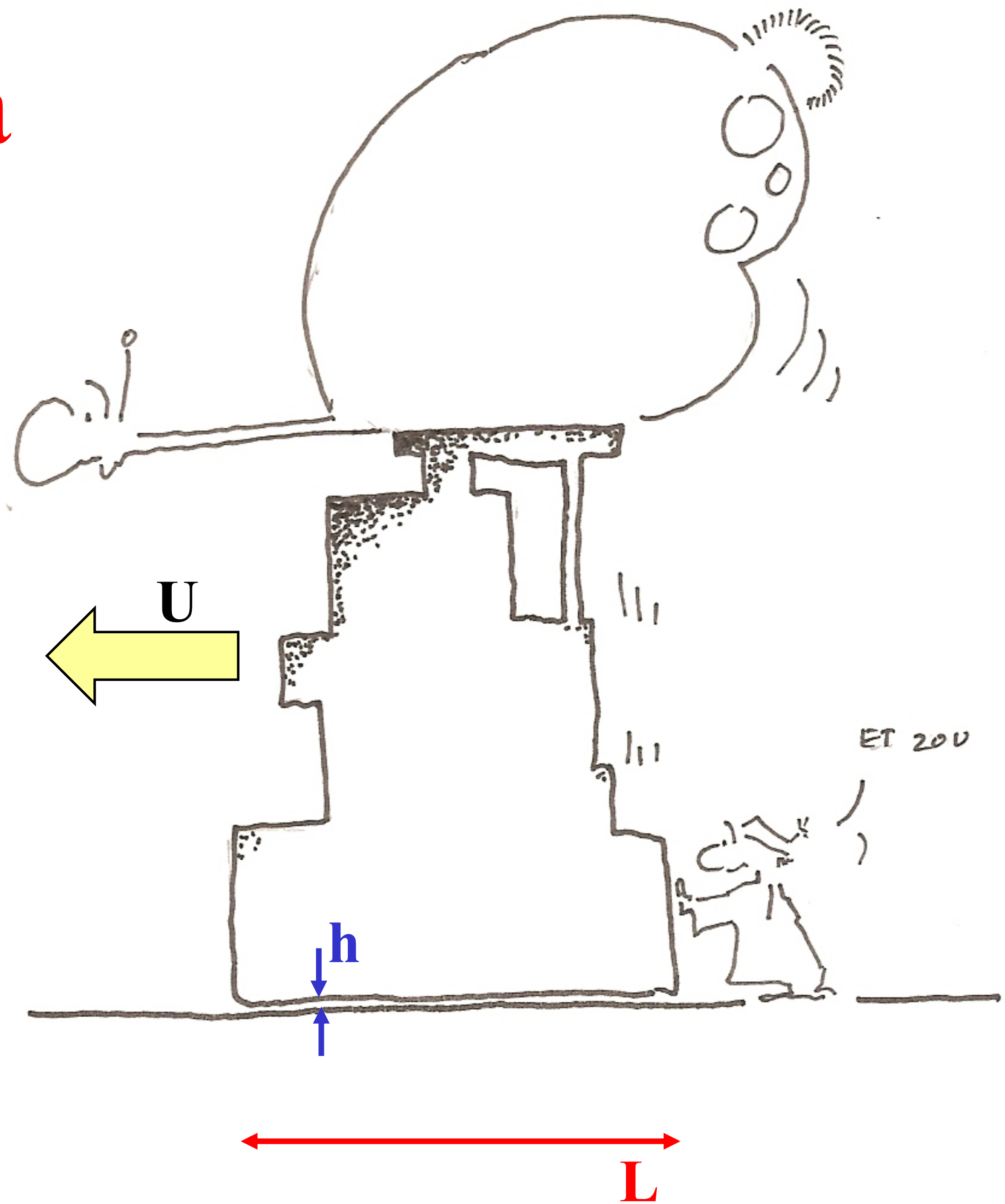




Convection naturelle le long d'une plaque verticale : écoulement laminaire permanent

Lubrification et convoyage hydraulique : butée Michell

Théorie de la lubrification



Convoyage hydraulique de charges très importantes :

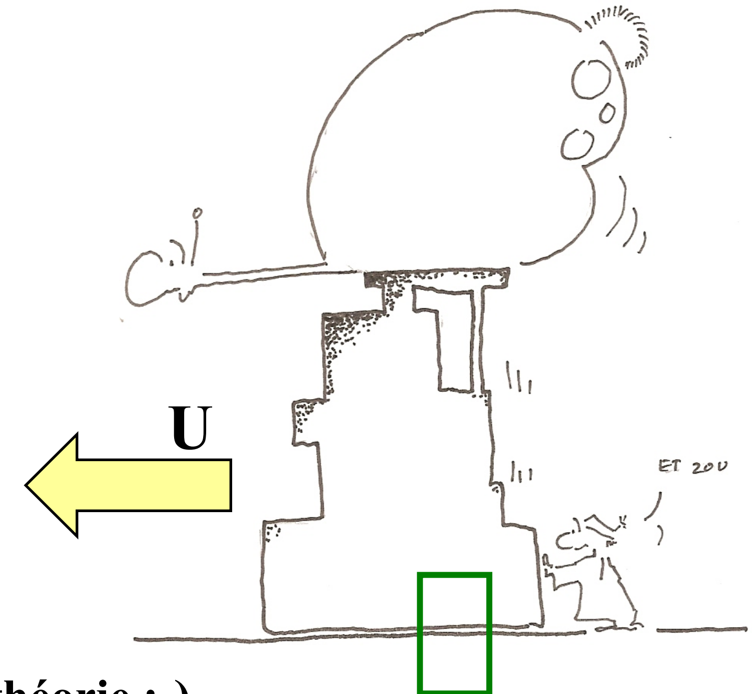
- turbines hydroélectriques

- applications marines

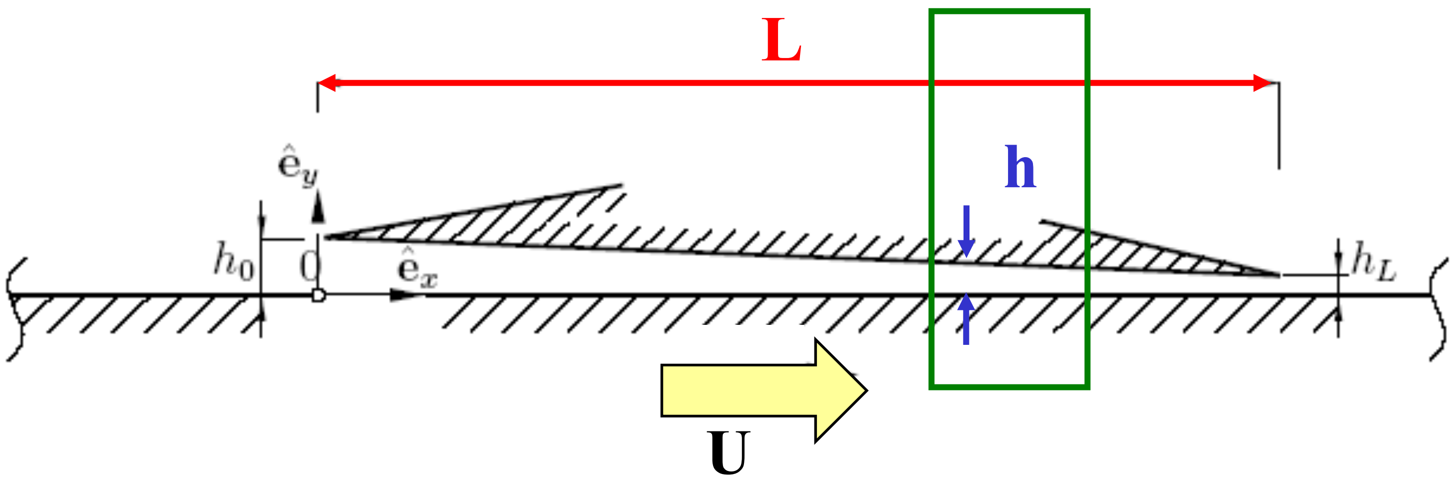
- butées hydrauliques

Théorie de la lubrification

$$\boxed{h \ll L}$$

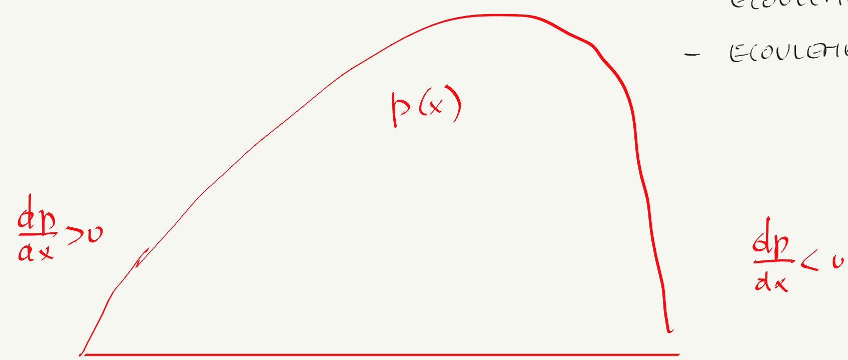


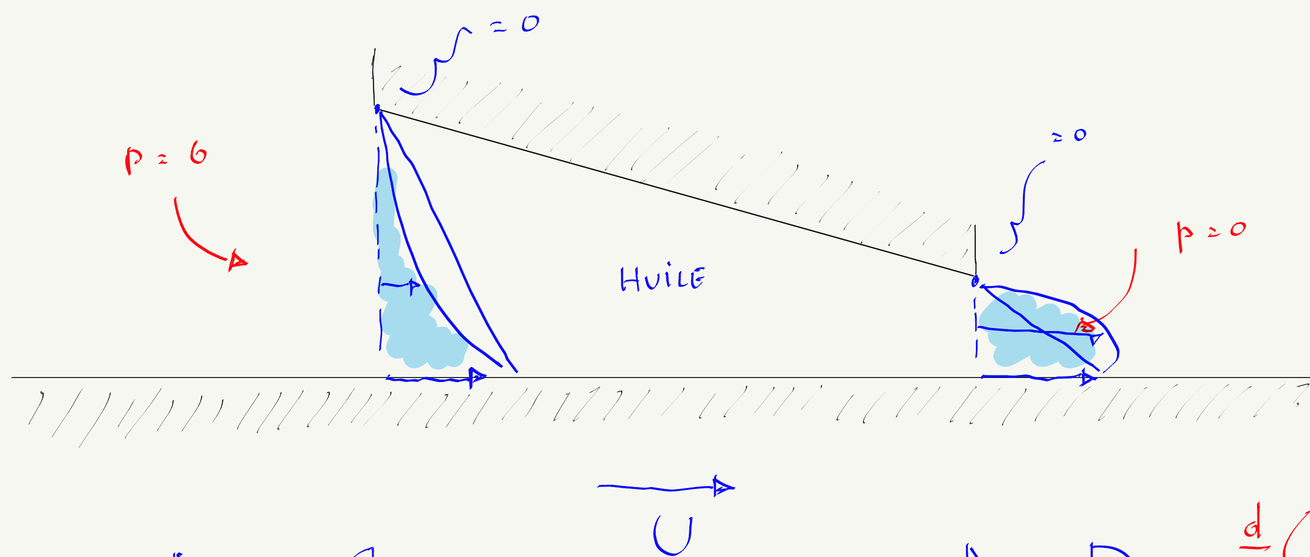
Hypothèse géométrique de base
Valable dans la zone centrale uniquement en théorie :-)

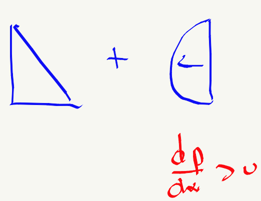


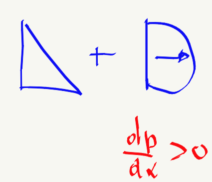
$\boxed{1}$ INTUITIVEMENT ?

- ECOULEMENT INCOMPRESSIBLE
- ECOULEMENT STATIONNAIRE









$$\frac{d}{dx}\big(\underbrace{Q(x)}_{\text{CONSTANTE}}\big) = 0$$

Ecoulements incompressibles plans stationnaires

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

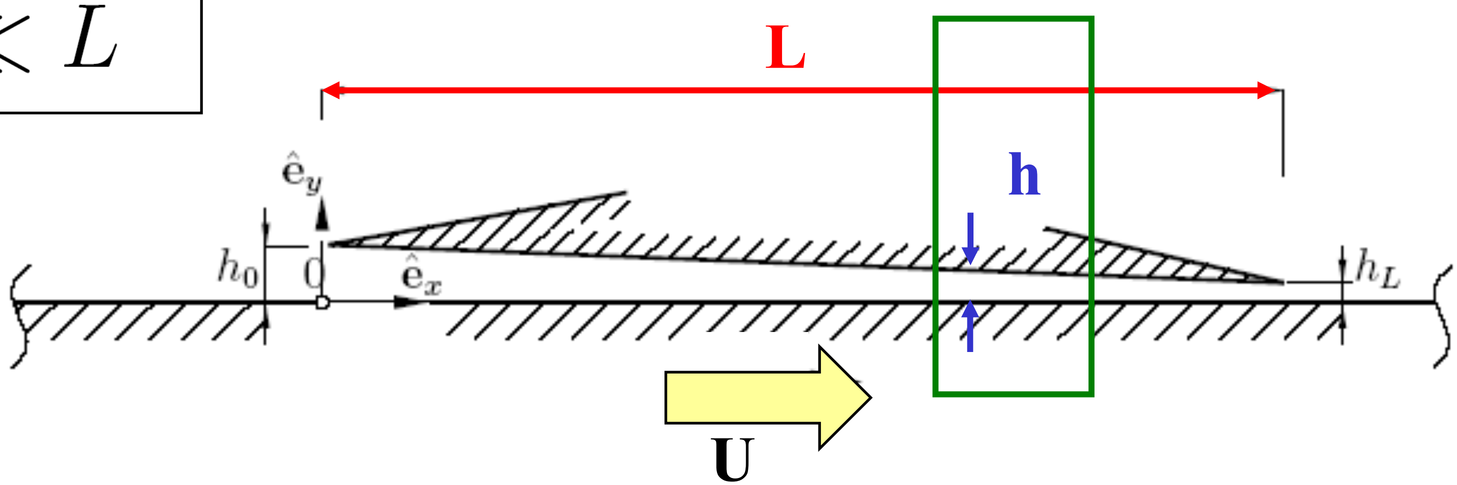
BILAN DE MASSE

$$\rho\, u \frac{\partial u}{\partial x} + \rho\, v \frac{\partial u}{\partial y} = -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial x^2} + \mu \frac{\partial^2 u}{\partial y^2}$$

$$\rho\, u \frac{\partial v}{\partial x} + \rho\, v \frac{\partial v}{\partial y} = -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial x^2} + \mu \frac{\partial^2 v}{\partial y^2}$$

Que deviennent ces équations ?

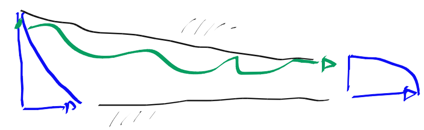
$$\boxed{h \ll L}$$

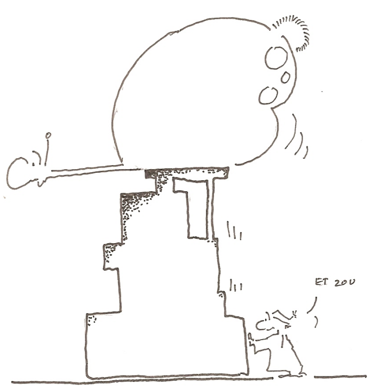


$$\boxed{h \ll L}$$

$$\begin{aligned}
\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} &= 0 \\
\rho\, u \frac{\partial u}{\partial x} + \rho\, v \frac{\partial u}{\partial y} &= -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial x^2} + \mu \frac{\partial^2 u}{\partial y^2} \\
\rho\, u \frac{\partial v}{\partial x} + \rho\, v \frac{\partial v}{\partial y} &= -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial x^2} + \mu \frac{\partial^2 v}{\partial y^2}
\end{aligned}$$

Longueur horizontale caractéristique : L
Longueur verticale caractéristique : h
Vitesse horizontale caractéristique : U





Comment choisir une vitesse verticale caractéristique ?

$\boxed{2}$

DEFINIR
UNE VITESSE
VERTICALE
CARACTERISTIQUE :-)

JE L'AI DEDUIT DE $h \ll L$

$$\boxed{\frac{\partial u}{\partial x}} + \boxed{\frac{\partial v}{\partial y}} = 0$$

$V \ll U$

CECI N'EST PAS UNE HYPOTHESE !

$$\frac{U}{L} = \frac{V}{h}$$

$$\boxed{V = \underbrace{\frac{h}{L}}_{\ll 1} U \ll U}$$

$$\underbrace{\frac{\partial u}{\partial x}}_{\mathcal{O}(U/L)} + \underbrace{\frac{\partial v}{\partial y}}_{\mathcal{O}(V/h)} = 0$$

Il ne faut pas définir de vitesse caractéristique verticale !

$$\boxed{V = \frac{Uh}{L} \ll U}$$

3 SIMPLIFIONS !

$$\underbrace{\cancel{\rho u \frac{\partial u}{\partial x}}}_{\mathcal{O}\left(\rho \frac{U^2}{L}\right)} + \underbrace{\cancel{\rho v \frac{\partial u}{\partial y}}}_{\mathcal{O}\left(\rho \frac{VU}{h}\right)} = -\frac{\partial p}{\partial x} + \underbrace{\cancel{\mu \frac{\partial^2 u}{\partial x^2}}}_{\mathcal{O}\left(\mu \frac{U}{L^2}\right)} + \underbrace{\mu \frac{\partial^2 u}{\partial y^2}}_{\mathcal{O}\left(\mu \frac{U}{h^2}\right)}$$

$$\mathcal{O}\left(\mu \frac{U}{L^2}\right) \ll \mathcal{O}\left(\mu \frac{U}{h^2}\right)$$

$$\underbrace{\mathcal{O}\left(\rho \frac{VU}{h}\right)}_{V = \frac{h}{L} U}$$

$$\mathcal{O}\left(\rho \frac{\cancel{h}}{L} U \frac{U}{\cancel{h}}\right) = \mathcal{O}\left(\rho \frac{U^2}{L}\right)$$

$$\frac{\text{INERTIE}}{\text{DIFFUSION}} = \frac{\rho\, U^2/L}{\mu\, U/h^2} = \underbrace{\frac{\rho\, U L}{\mu}}_{Re} \underbrace{\frac{h^2}{L^2}}_{\ll 1} \ll 1$$

EN SUPPOSANT QUE Re RESTE RAISONNABLE

Quand peut-on négliger les termes d'inertie ?

$$\overset{\mathcal{O}(\rho U^2/L)}{\boxed{\cancel{\rho\, u \frac{\partial u}{\partial x}}}} + \underset{\mathcal{O}(\rho V U/h)}{\overset{\mathcal{O}(\rho U^2/L)}{\boxed{\cancel{\rho\, v \frac{\partial u}{\partial y}}}}} = -\frac{\partial p}{\partial x} + \boxed{\cancel{\mu \frac{\partial^2 u}{\partial x^2}}} + \boxed{\mu \frac{\partial^2 u}{\partial y^2}}$$

$$\mathcal{O}(\mu U/L^2) \ll \mathcal{O}(\mu U/h^2)$$

Hypothèse de lubrification :
Écoulements rampants

$$\frac{\boxed{\text{Forces d'inertie}}}{\boxed{\text{Forces visqueuses}}} = \frac{\rho U^2/L}{\mu U/h^2} = \underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

Et l'autre équation ?

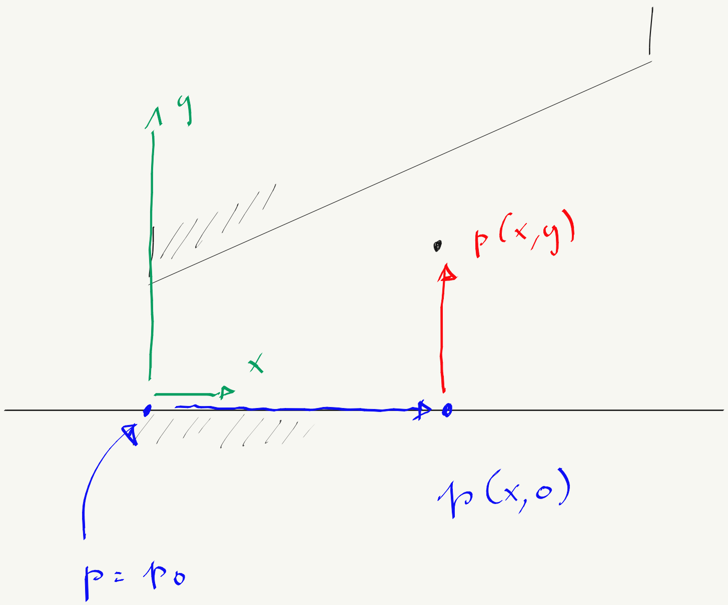
$$\overset{\mathcal{O}(\rho U^2 h/L^2)}{\boxed{\cancel{\rho\, u \frac{\partial v}{\partial x}}}} + \overset{\mathcal{O}(\rho U^2 h/L^2)}{\boxed{\cancel{\rho\, v \frac{\partial v}{\partial y}}}} = -\frac{\partial p}{\partial y} + \boxed{\cancel{\mu \frac{\partial^2 v}{\partial x^2}}} + \boxed{\mu \frac{\partial^2 v}{\partial y^2}}$$

$$\mathcal{O}(\mu U h/L^3) \ll \mathcal{O}(\mu U/Lh)$$

On obtient la même condition…

$$\frac{\boxed{\text{Forces d'inertie}}}{\boxed{\text{Forces visqueuses}}} = \frac{\rho U^2 h/L^2}{\mu U/Lh} = \underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

4 ET LA PRESSION ?



$$\mathcal{O}\left(\cancel{h}\,\mu\,\frac{U\cancel{h}}{L}\,\frac{1}{\cancel{h^2}}\right)$$

$$\mathcal{O}(h) \qquad \mathcal{O}\left(\mu\frac{V}{h^2}\right)$$

$$p(x,y) - p_0 = \boxed{p(x,0) - p_0} + \boxed{y\,\frac{\partial p}{\partial y}\Big|_{y=0}} + \underbrace{y^2\ \cdots\cdots}_{\text{C'EST PETIT CAR } y^2 \ll y\ :-)}$$

$$x\,\frac{\partial p}{\partial x}$$

$$\mathcal{O}(L) \qquad \mathcal{O}\left(\mu\frac{U}{h^2}\right)$$

$$\partial\left(\cancel{h}\,\mu\,\frac{U\cancel{h}}{L}\,\frac{1}{\cancel{h^2}}\right)$$

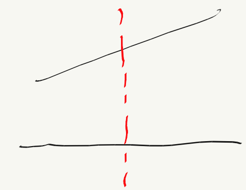
$$\partial(h) \qquad \partial\left(\mu\frac{V}{h^2}\right)$$

$$p(x,y)-p_0=\boxed{p(x,0)-p_0}+\cancel{\boxed{y\left.\frac{\partial p}{\partial y}\right|_{y=0}}}+\underbrace{y^2\;\cdots}$$

C'EST PETIT CAR $y^2 \ll y$:-)

$$x\,\frac{\partial p}{\partial x}$$

$$\partial(L) \qquad \partial\left(\mu\frac{U}{h^2}\right)$$



$p(x)$:-)

LA PRESSION NE DEPEND PAS DE y !

$$\boxed{\mu\frac{UL}{h^2}} \gg \boxed{\mu\frac{U}{L}=\mu\frac{UL}{L^2}}$$

$$\mu UL \gg \mu UL\,\underbrace{\frac{h^2}{L^2}}_{\ll 1}$$

REYNOLDS

$$\frac{\partial u}{\partial x}+\frac{\partial v}{\partial y}=0$$

$$\frac{dp}{dx}=\mu\frac{\partial^2 u}{\partial y^2}$$

THEORIE DE LA LUBRIFICATION

$$\boxed{\cancel{\rho\, u \frac{\partial v}{\partial x}}} + \boxed{\cancel{\rho\, v \frac{\partial v}{\partial y}}} = -\frac{\partial p}{\partial y} + \boxed{\cancel{\mu \frac{\partial^2 v}{\partial x^2}}} + \boxed{\mu \frac{\partial^2 v}{\partial y^2}}$$

$$\mathcal{O}(\mu U / L h)$$

Et la pression ?

$$p(x,y) - p_0 = \boxed{p(x,0) - p_0} + \boxed{y \cancel{\frac{\partial p}{\partial y}}\Big|_{y=0}}$$

$p(x)$:-)

$$\mathcal{O}(\mu U L / h^2) \gg \mathcal{O}(\mu U L / L^2)$$

$$\mathcal{O}(\mu U / h^2)$$

$$\boxed{\cancel{\rho\, u \frac{\partial u}{\partial x}}} + \boxed{\cancel{\rho\, v \frac{\partial u}{\partial y}}} = -\frac{\partial p}{\partial x} + \boxed{\cancel{\mu \frac{\partial^2 u}{\partial x^2}}} + \boxed{\mu \frac{\partial^2 u}{\partial y^2}}$$

Equations de Reynolds (1889)

Théorie de la lubrification

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$0 = -\frac{dp}{dx} + \mu \frac{\partial^2 u}{\partial y^2}$$

Film fluide mince

$$h \ll L$$

Hypothèse de lubrification :
Écoulements rampants

$$\underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

Est-ce que l'hypothèse de lubrification est réaliste ?

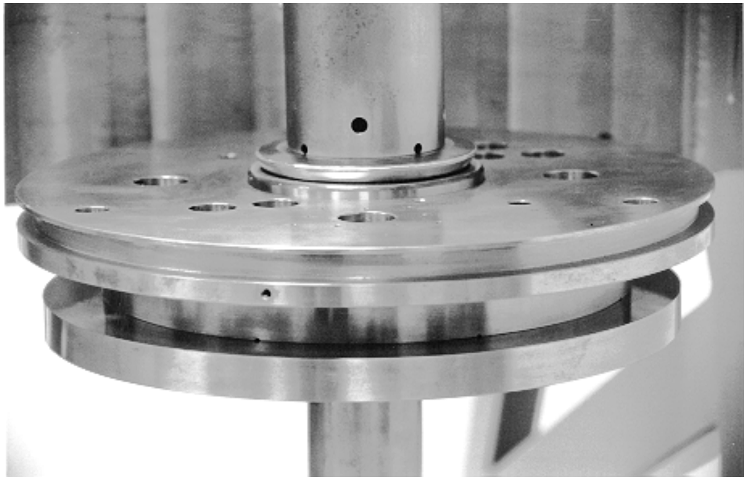
$$\underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

0.0375

$$\begin{array}{rcl} L & = & 10\ cm \\ h & = & 0.5\ mm \\ U & = & 1\ m/s \end{array}$$

$$\begin{array}{rcl} \rho & = & 900\ kg/m^3 \\ \mu & = & 60\ 10^{-3}\ Ns/m^2 \end{array}$$

Huile SAE50 à 60 degrés



Huile SAE 50
C'est quoi ?

Transport maritime

Marine LCX

Une huile formulée spécialement pour la lubrification des gros moteurs diesel marins à crosse. Elle lubrifie les cylindres grâce à un indice de basicité très élevé de 70 et un grade SAE* 50.

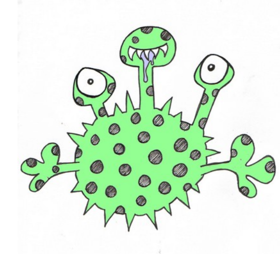
Grades offerts :
SAE 50

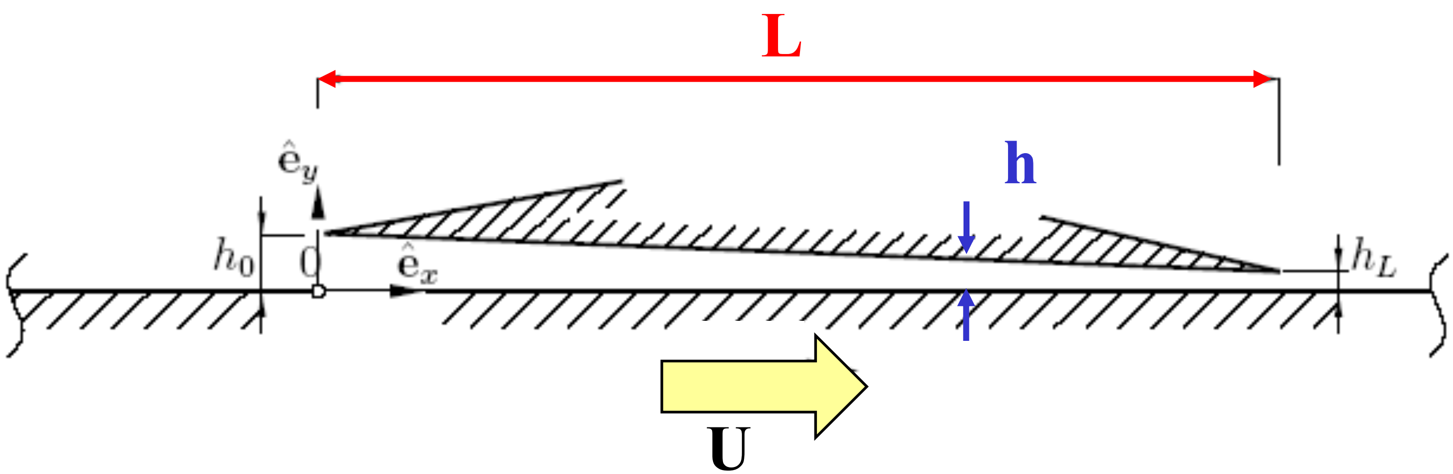
Fiche technique
Fiche signalétique

-i- calcul de u(x,y)

$$\left\{\begin{array}{rcl} \boxed{\dfrac{\partial u}{\partial x} + \dfrac{\partial v}{\partial y} = 0} \\ \boxed{-\dfrac{dp}{dx} + \mu \dfrac{\partial^2 u}{\partial y^2} = 0} \end{array}\right.$$

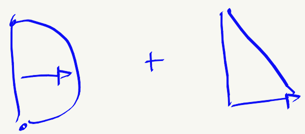
$$\boxed{u(x,y) = -\frac{dp}{dx}\,\frac{h^2}{2\mu}\,\frac{y}{h}\left(1 - \frac{y}{h}\right) + U\left(1 - \frac{y}{h}\right)}$$



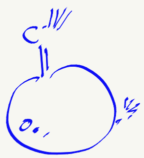


5 CALCUL DU PROFIL DE VITESSE :-)

$$\frac{dp}{dx} = \mu \frac{\partial^2 u}{\partial y^2}$$



$$\boxed{u(x,y) = \underbrace{-\frac{dp}{dx}\,\frac{h^2}{2\mu}}\left(1-\frac{y}{h}\right)\frac{y}{h} + U\left(1-\frac{y}{h}\right)}$$



$$\left[\frac{\cancel{N}}{m^3}\right]\left[\frac{m^2}{\cancel{N}\,s/m^2}\right] = \left[\frac{m^4}{m^3\,s}\right] = \left[\frac{m}{s}\right] \quad :-)$$

$$\tau = 2\mu\, d$$

$$\left[\frac{N}{m^2}\right] \qquad \left[\frac{N\,s}{m^2}\right] \qquad \left[\frac{1}{s}\right]$$

$\boxed{6}$ **CALCUL DE LA PRESSION**

(*) $$\int_0^h \frac{y}{h} - \frac{y^2}{h^2}\, dy$$

$$= \left[\frac{y^2}{2h} - \frac{y^3}{3h^2} \right]_0^h = \frac{h}{2} - \frac{h}{3}$$

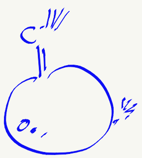
$$= \frac{3h - 2h}{6} = \frac{h}{6}$$:-)

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$0 = \int_0^h \frac{\partial u}{\partial x}\, dy + \int_0^h \frac{\partial v}{\partial y}\, dy$$

$$= \frac{d}{dx} \underbrace{\int_0^h u\, dy}_{Q(x)} + \underbrace{\left[v \right]_0^h}_{=0}$$

$$\boxed{u(x,y) = -\frac{dp}{dx}\frac{h^2}{2\mu}\left(1-\frac{y}{h}\right)\frac{y}{h} + U\left(1-\frac{y}{h}\right)}$$



$$0 = \frac{d}{dx}\left[-\frac{dp}{dx}(x)\,\frac{h^2(x)}{2\mu} \underbrace{\int_0^{h(x)} \left(1-\frac{y}{h(x)}\right)\left(\frac{y}{h(x)}\right) dy}_{\frac{h(x)}{6}} + U\,\frac{h(x)}{2} \right]$$

:-) (*)

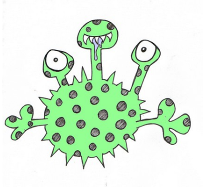
-ii- calcul de p(x)

$$\left\{\begin{array}{rcl} \boxed{-\dfrac{dp}{dx} + \mu\dfrac{\partial^2 u}{\partial y^2} = 0} \\ \boxed{\dfrac{\partial u}{\partial x} + \dfrac{\partial v}{\partial y} = 0} \end{array}\right.$$

$$0 = \int_0^h \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} dy$$

$$0 = \frac{d}{dx}\overbrace{\int_0^h u(x,y)dy}^{Q(x)} + \cancel{\left[v(x,y) \right]_0^h}$$

En utilisant l'expression de u(x,y)



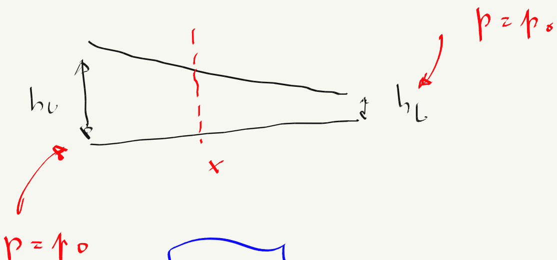
Equation classique de Reynolds (1889)

$$0 = \frac{d}{dx}\left(-\frac{dp}{dx}\frac{h^3}{12\mu} + \frac{Uh}{2}\right)$$

$$0 = \frac{d}{dx}\left[-\frac{dp}{dx}(x)\,\frac{h^2(x)}{2\mu}\underbrace{\int_0^{h(x)}\left(1-\frac{y}{h(x)}\right)\left(\frac{y}{h(x)}\right)dy}_{h(x)/6} + U\,\frac{h(x)}{2}\right]$$

$$0 = \frac{d}{dx}\left[-\frac{dp}{dx}(x)\,\frac{h^3(x)}{12\mu} + U\,\frac{h(x)}{2}\right]$$

$$\frac{dh}{dx} = \frac{h_L-h_0}{L}$$



$$\frac{d}{dx}\left[\frac{dp}{dx}(x)\,h^3(x)\right] = 6\mu U\,\frac{dh}{dx}$$

$$\left(\frac{dh}{dx}\right)^2 \frac{d}{dh}\left[\frac{dp}{dh}(h)\,h^3\right] = 6\mu U\,\frac{h_L-h_0}{L}$$

$$\left(\frac{h_L-h_0}{L}\right)^2$$

$$-\frac{d}{dh}\left[\frac{dp}{dh}\,h^3\right] = \underbrace{\frac{6\mu U L}{h_0-h_L}}_{C}$$

$$-\frac{dp}{dh}\,h^3 = C\left[h+A\right]$$

$$-\frac{dp}{dh} = C\left[\frac{1}{h^2}+\frac{A}{h^3}\right]$$

$$p(h) = C\left[\frac{1}{h}+\frac{A}{2h^2}+B\right]$$

$$0 = \frac{d}{dx}\left(-\frac{dp}{dx}\frac{h^3}{12\mu} + \frac{Uh}{2}\right)$$

$$\frac{d}{dx}\left(h^3(x)\,\frac{dp}{dx}(x)\right) = 6\mu U \boxed{\frac{dh}{dx}}$$

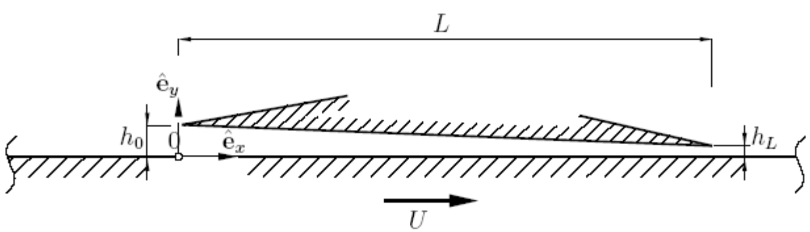
$$-\frac{d}{dh}\left(h^3\frac{dp}{dh}(h)\right) = \frac{6\mu U L}{h_0 - h_L}$$

$$-h^3\frac{dp}{dh}(h) = \frac{6\mu U L}{h_0 - h_L}(h + A)$$

$$-\frac{dp}{dh}(h) = \frac{6\mu U L}{h_0 - h_L}\left(\frac{1}{h^2} + \frac{A}{h^3}\right)$$

$$p(h) = \frac{6\mu U L}{h_0 - h_L}\left(B + \frac{1}{h} + \frac{A}{2h^2}\right)$$

Palier plat

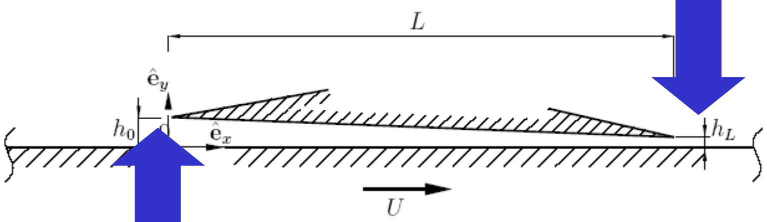


$$\frac{x}{L} = \frac{h_0 - h(x)}{h_0 - h_L}$$

$$\frac{dh}{dx} = -\frac{h_0 - h_L}{L}$$

$$p(h_L) = p_0$$

Deux conditions aux limites



$$p(h_0) = p_0$$

Deux constantes

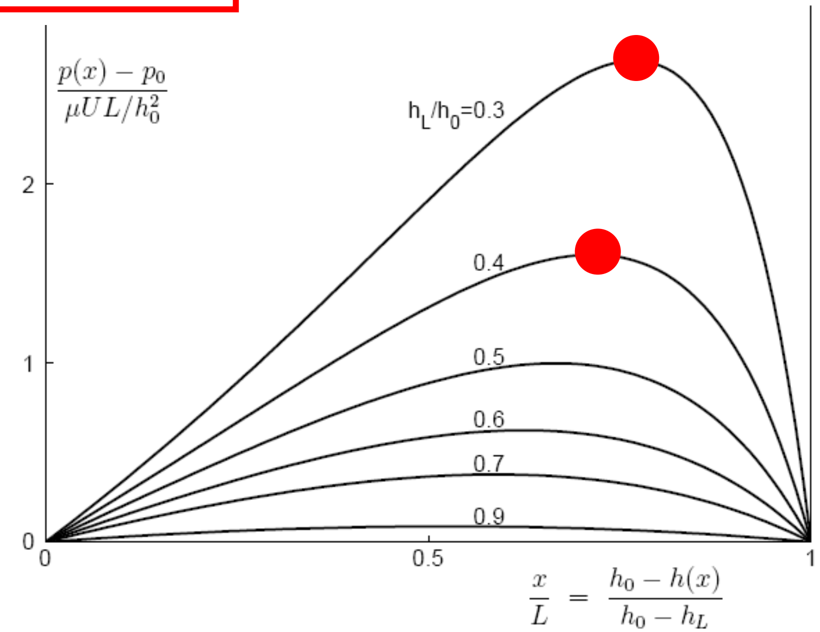
$$p(h) = \frac{6\mu U L}{h_0 - h_L}\left(\boxed{B} + \frac{1}{h} + \frac{\boxed{A}}{2h^2}\right)$$

$$\downarrow$$

$$p(h) - p_0 = \frac{6\mu U L (h_0 - h)(h - h_L)}{(h_0^2 - h_L^2)h^2}$$

$$\boxed{h = \frac{2\,h_0\,h_L}{(h_0 + h_L)}}$$

Où la pression est-elle maximale ?

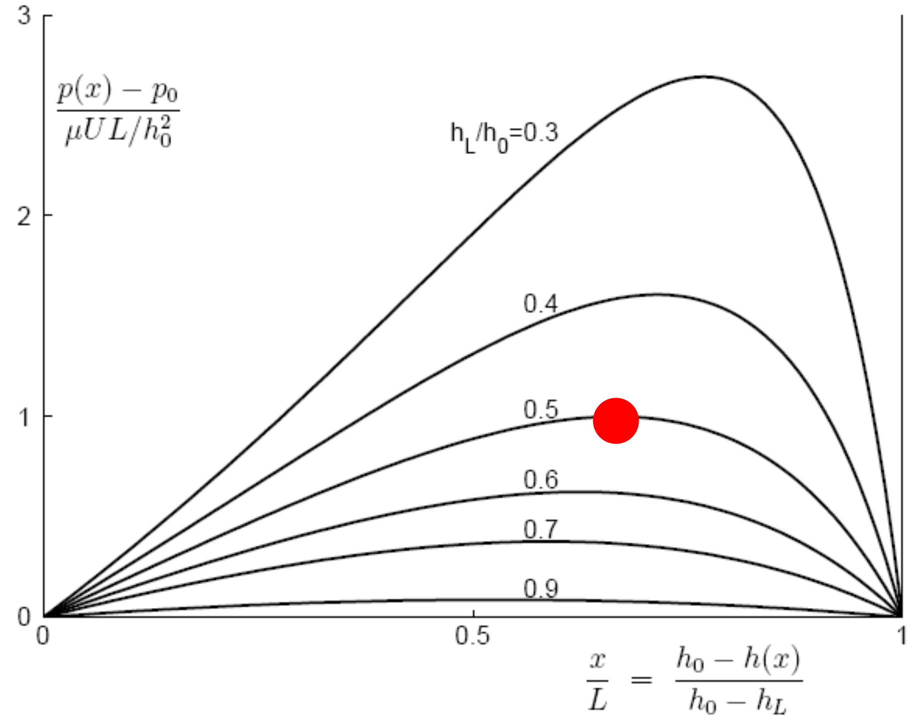


Cette pression peut être énorme !

$$
\begin{aligned}
L &= 10\ cm \\
h_0 &= 0.1\ mm \\
h_L &= 0.05\ mm \\
U &= 10\ m/s
\end{aligned}
$$

$$
\begin{aligned}
\rho &= 900\ kg/m^3 \\
\mu &= 0.1\ Ns/m^2
\end{aligned}
$$

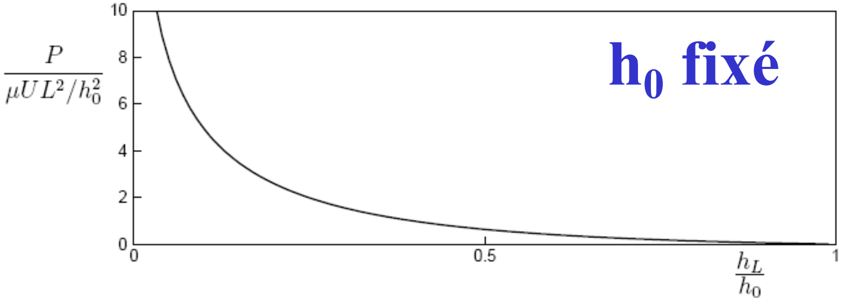
Huile SAE50 à 50 degrés

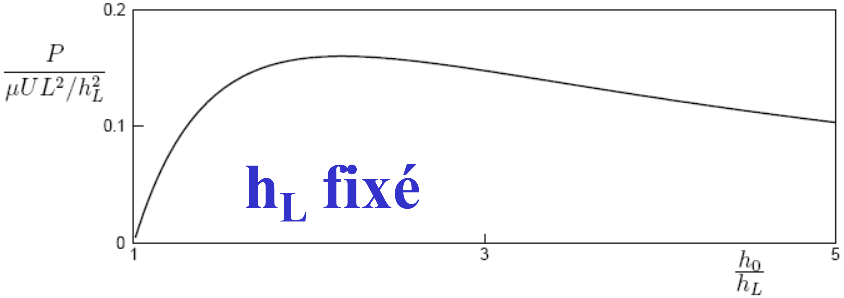


$$p_{\max} - p_0 = \boxed{\frac{3}{2}\frac{\mu U L}{h_0 h_L}\frac{(h_0 - h_L)}{(h_0 + h_L)}}$$

10^7 Pascal

Charge utile

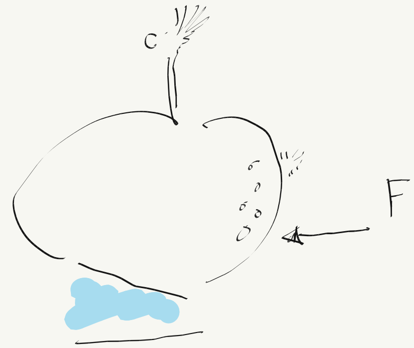


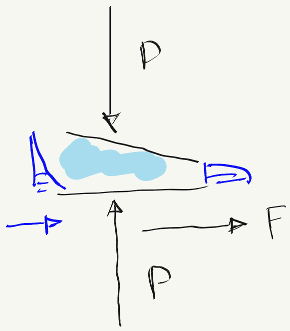


$$
\begin{aligned}
P &= \int_0^L (p(x) - p_0)\, dx \\
&= -\frac{L}{(h_0 - h_L)} \int_{h_0}^{h_L} (p(h) - p_0)\, dh \\
&= -\frac{L}{(h_0 - h_L)} \frac{6\,\mu\, U\, L}{(h_0^2 - h_L^2)} \int_{h_0}^{h_L} \left[(h_0 + h_L)\frac{1}{h} - \frac{h_0\, h_L}{h^2} - 1\right] dh \\
&= -6\,\mu\, U\, L^2 \left[\frac{1}{(h_0 - h_L)^2} \log\left(\frac{h_L}{h_0}\right) + \frac{2}{(h_0^2 - h_L^2)}\right]
\end{aligned}
$$

CHARGE
UTILE

$$P = \int_0^L p(x) - p_0 \, dx$$



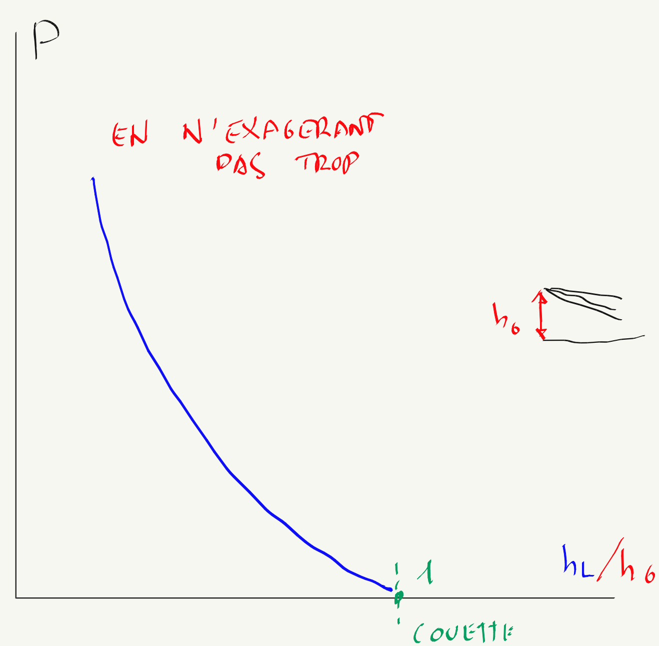


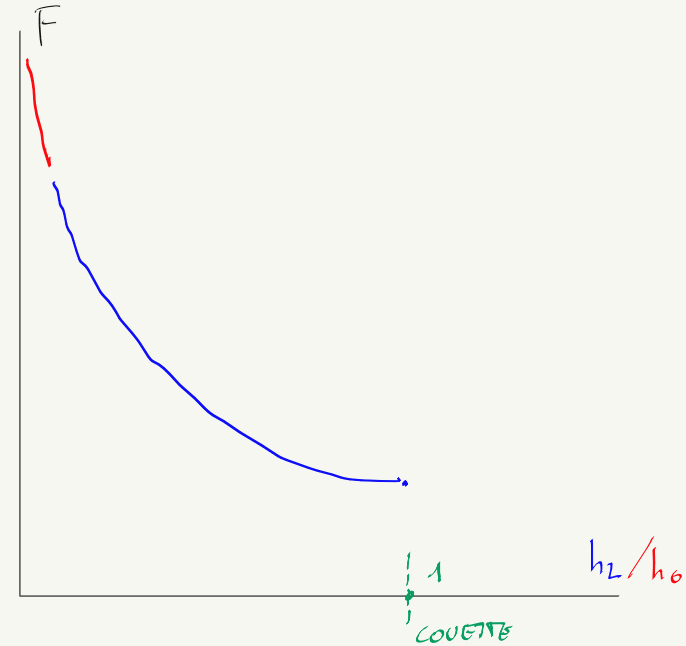
FORCE
DE POUSSÉE

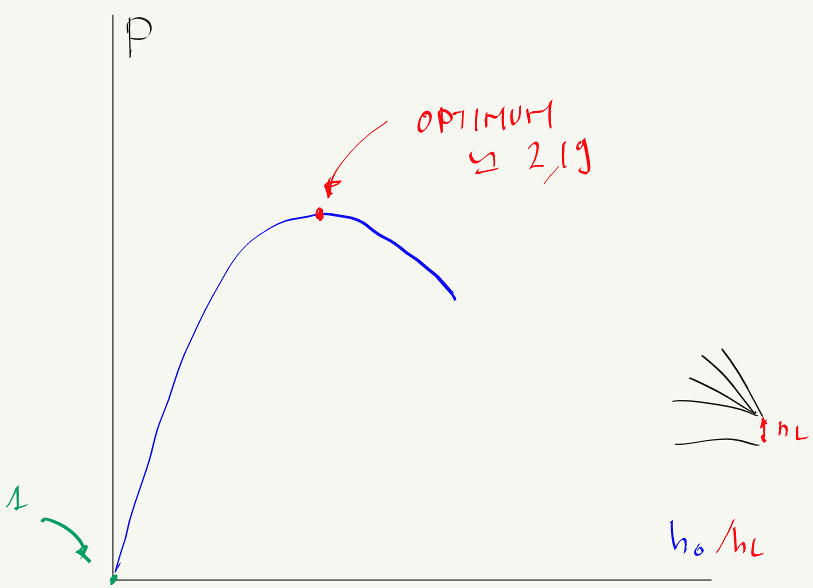
$$F = -\mu \int_0^L \frac{\partial u}{\partial y} \, dx$$

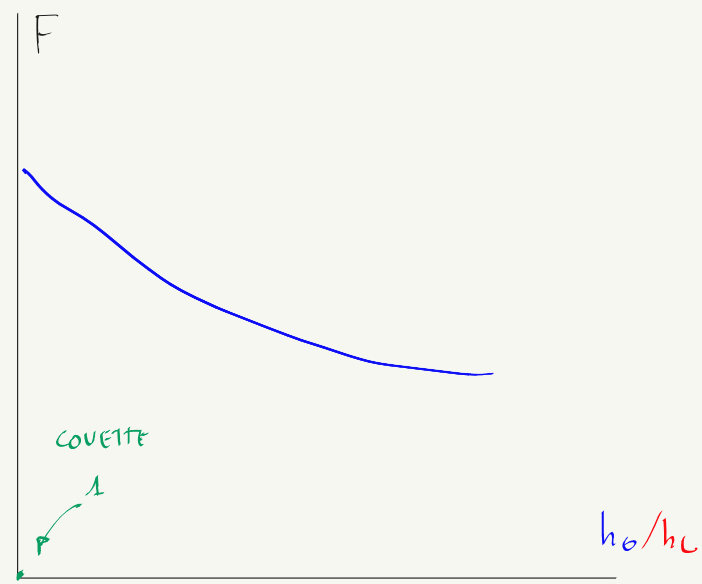
PUISSANCE
DISSIPÉE :-)

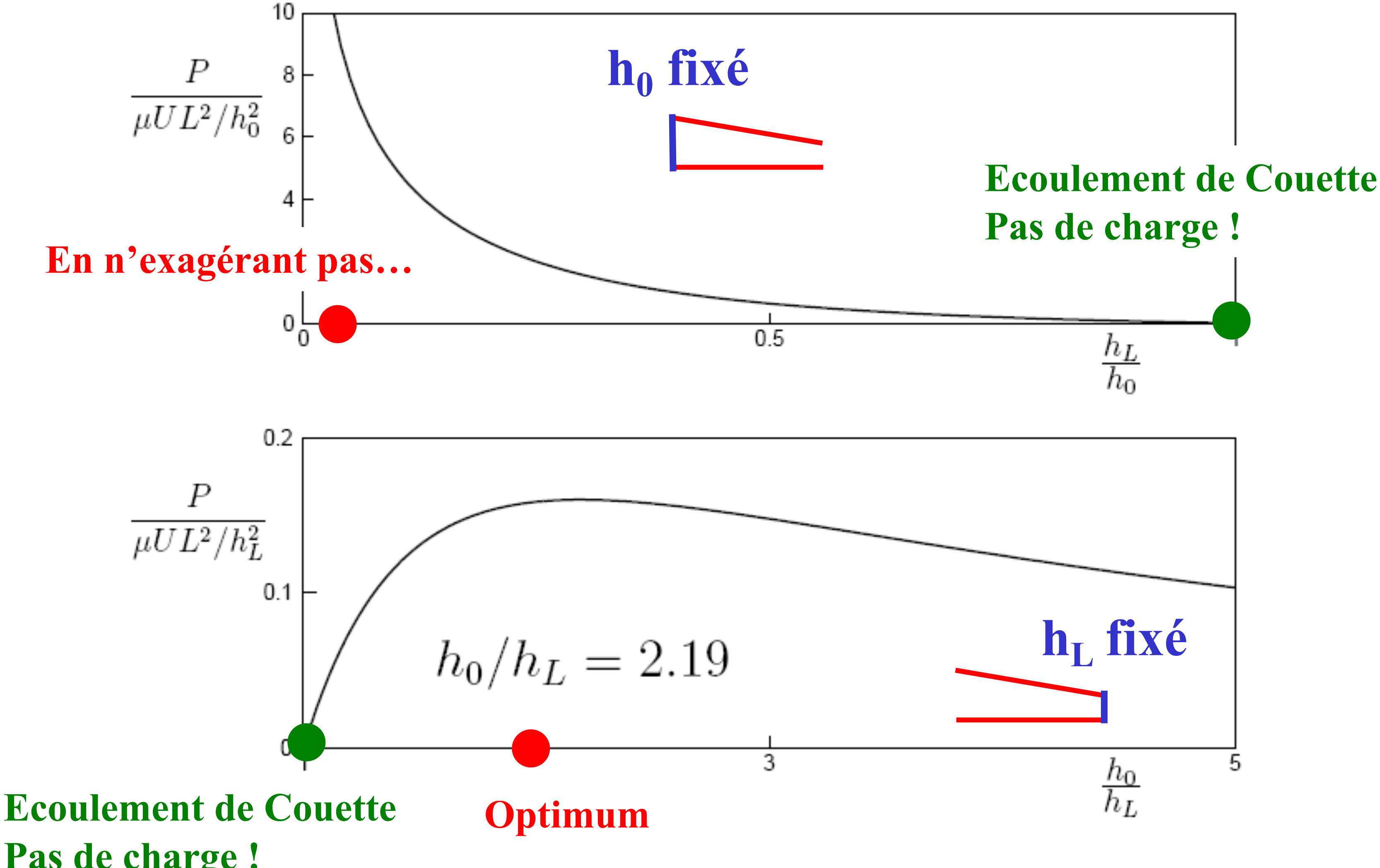
$$= F \cdot U$$


P
EN N'EXAGERANT PAS TROP
h_0
h_L / h_0
1
COUETTE


F
h_L / h_0
1
COUETTE

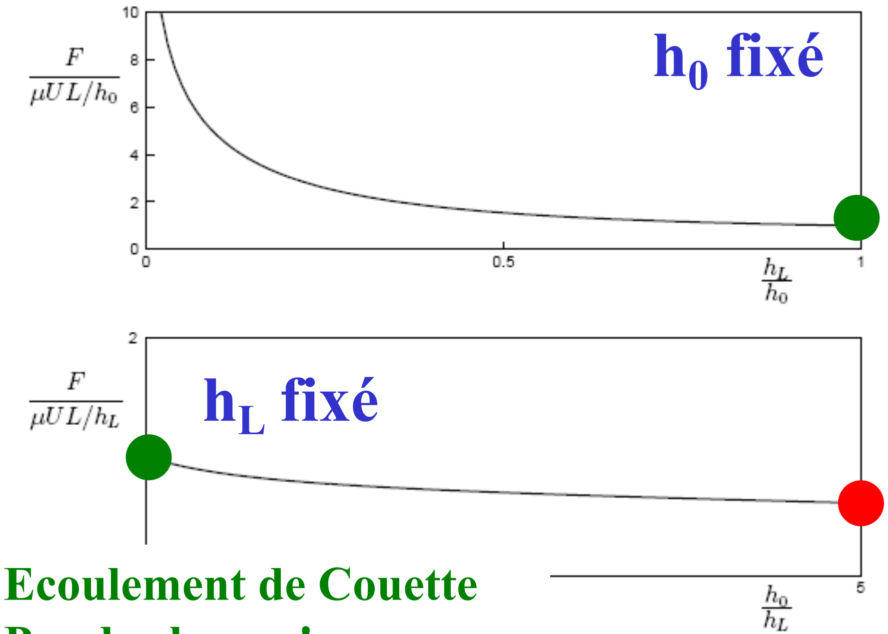

P
OPTIMUM ≃ 2,19
h_L
h_0 / h_L
1


F
COUETTE
1
h_0 / h_L



Rapport optimal…

Force exercée par le fluide sur la partie mobile



Ecoulement de Couette
Pas de charge !

La force diminue de façon monotone lorsque le rapport augmente…

$$
\begin{aligned}
F &= -\int_0^L \mu \left.\frac{\partial u}{\partial y}\right|_{y=0} dx \\
&= \frac{\mu U L}{(h_0 - h_L)} \int_{h_0}^{h_L} \left[\frac{6}{h^2} \frac{h_0 \, h_L}{(h_0 + h_L)} - \frac{4}{h} \right] dh \\
&= -\mu U L \left[\frac{6}{(h_0 + h_L)} + \frac{4}{(h_0 - h_L)} \log\left(\frac{h_L}{h_0} \right) \right]
\end{aligned}
$$

La puissance consommée est dissipée…

$$F\,U = -\frac{\mu\,U^2\,L}{h_0}\left[\frac{6}{(1+h_L/h_0)} + \frac{4}{(1-h_L/h_0)}\log\left(\frac{h_L}{h_0}\right)\right]$$

Embêtant…

S’assurer que l’huile est bien refroidie car la viscosité (et donc la charge utile) décroît rapidement avec la température…

…en chaleur !

A propos de la viscosité de notre huile SAE 50

Transport maritime

Marine LCX

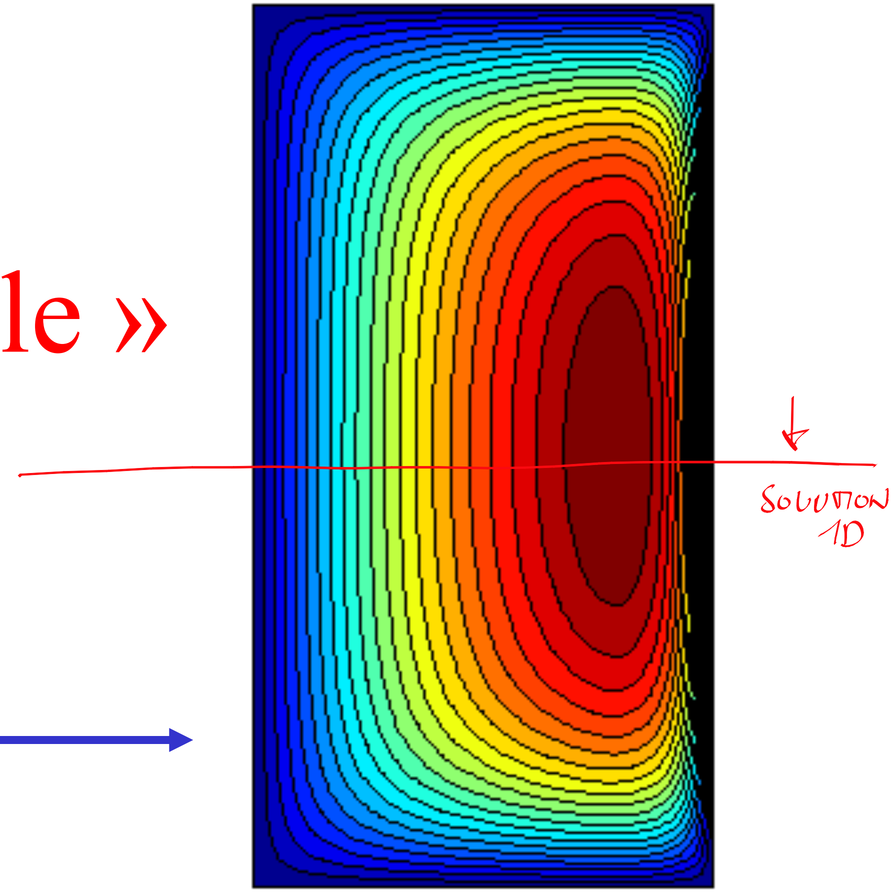
Une huile formulée spécialement pour la lubrification des gros moteurs diesel marins à crosse. Elle lubrifie les cylindres grâce à un indice de basicité très élevé de 70 et un grade SAE* 50.

Grades offerts :
SAE 50

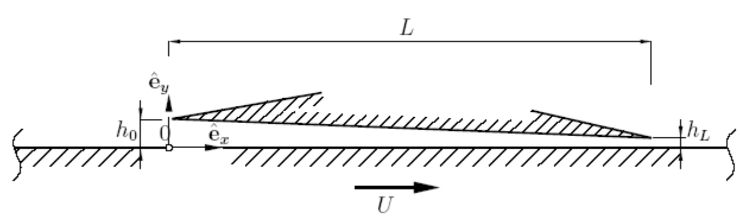
Fiche techniqu
Fiche signalét

$$
\begin{aligned}
T &= 20^0 C & \mu &= 1.100\ Ns/m^2 \\
T &= 40^0 C & \mu &= 0.210\ Ns/m^2 \\
T &= 50^0 C & \mu &= 0.100\ Ns/m^2 \\
T &= 60^0 C & \mu &= 0.060\ Ns/m^2 \\
T &= 80^0 C & \mu &= 0.025\ Ns/m^2 \\
T &= 100^0 C & \mu &= 0.013\ Ns/m^2
\end{aligned}
$$

Analyse « tridimensionnelle » du palier plat



pression sous un palier dont la largeur vaut le double de la longueur



Lubrification 2D ½

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

$$\frac{\partial p}{\partial x} = \mu \frac{\partial^2 u}{\partial z^2}$$

$$\frac{\partial p}{\partial y} = \mu \frac{\partial^2 v}{\partial z^2}$$

$$\frac{\partial p}{\partial z} = 0$$

Théorie de la lubrification

Film fluide mince

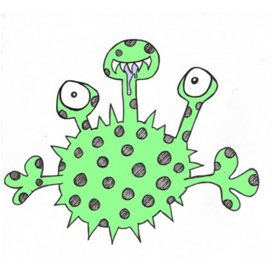
$$h \ll L$$

Hypothèse de lubrification : Écoulements rampants

$$\underbrace{\frac{\rho U L}{\mu}}_{Re_L} \frac{h^2}{L^2} \ll 1$$

-i- calcul de u(x,y,z) et de v(x,y,z)

$$\left\{\begin{array}{rcl} \boxed{\dfrac{\partial u}{\partial x} + \dfrac{\partial v}{\partial y} + \dfrac{\partial w}{\partial z} = 0} \\ -\dfrac{\partial p}{\partial x} + \mu \dfrac{\partial^2 u}{\partial z^2} &=& 0 \\ -\dfrac{\partial p}{\partial y} + \mu \dfrac{\partial^2 v}{\partial z^2} &=& 0 \end{array}\right.$$



$$u(x,y,z) = -\frac{\partial p}{\partial x}\frac{h^2}{2\mu}\frac{z}{h}\left(1-\frac{z}{h}\right) + U\left(1-\frac{z}{h}\right)$$

$$v(x,y,z) = -\frac{\partial p}{\partial y}\frac{h^2}{2\mu}\frac{z}{h}\left(1-\frac{z}{h}\right)$$

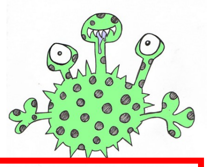
? C'EST NORMAL

-ii- calcul de p(x,y)

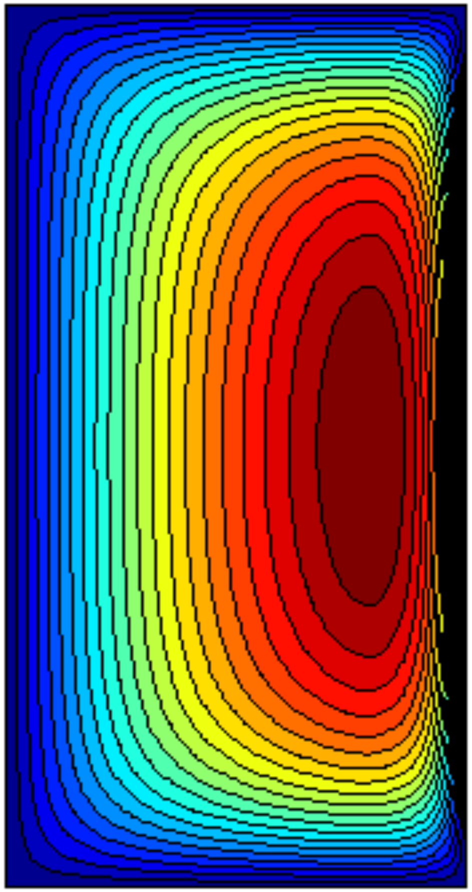
$$\left\{\begin{array}{rcl} \boxed{\begin{array}{rcl} -\dfrac{\partial p}{\partial x} + \mu \dfrac{\partial^2 u}{\partial z^2} & = & 0 \\ -\dfrac{\partial p}{\partial y} + \mu \dfrac{\partial^2 v}{\partial z^2} & = & 0 \end{array}} \\ \boxed{\dfrac{\partial u}{\partial x} + \dfrac{\partial v}{\partial y} + \dfrac{\partial w}{\partial z} = 0} \end{array}\right.$$

$$\int_0^h \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}\, dz = 0$$

$$\frac{\partial}{\partial x}\int_0^h u(x,y,z)dz + \frac{\partial}{\partial y}\int_0^h v(x,y,z)dz + \Big[\,\cancel{w(x,y,z)}\,\Big]_0^h = 0$$



$$\boxed{\frac{\partial}{\partial x}\left(h^3\frac{\partial p}{\partial x}\right) + \frac{\partial}{\partial y}\left(h^3\frac{\partial p}{\partial y}\right) = 6\mu U\frac{dh}{dx}}$$



-iiii- calcul numérique par différences finies de p(x,y)

$$h^3 \underbrace{\left(\frac{\partial^2 p}{\partial x^2} + \frac{\partial^2 p}{\partial y^2}\right)}_{\text{DIFFUSION}} + 3h^2 \overbrace{\left(\frac{h_L - h_0}{L}\right)}^{\text{TRANSPORT}} \frac{\partial p}{\partial x} = 6\mu U \left(\frac{h_L - h_0}{L}\right)$$